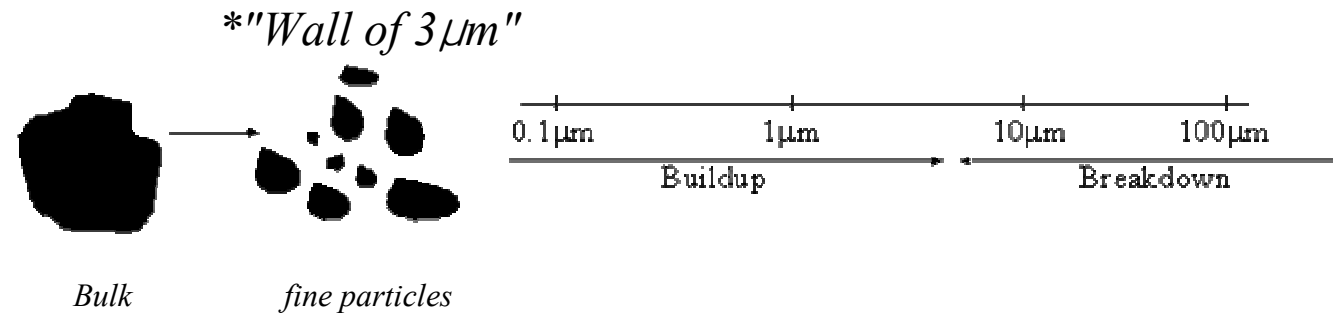


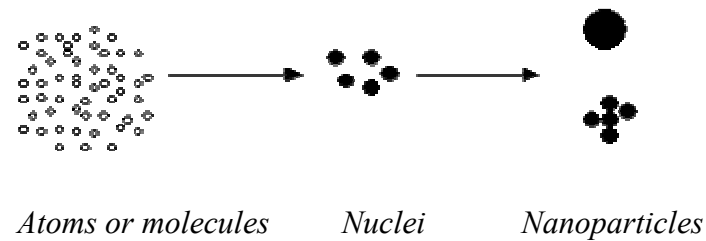
Chapter 4. Formation and Growth of Nanoparticles - Theories

4.1 Introduction

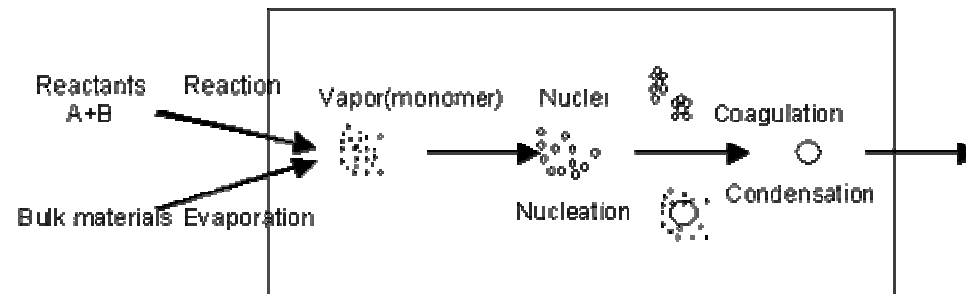
- Breakdown (Disintegration) : by crushing, milling, spraying



- Buildup (Growth) : nucleation and growth (condensation, coagulation)



*



4.2 Birth of Nanoparticles: Nucleation

Formation of nuclei: new-born particles

(1) Homogeneous nucleation

- Gibbs free energy change for a droplet from monomer molecules

$$\Delta G = \underbrace{\pi d_p^2 \sigma}_{\text{interfacial energy}} - \underbrace{\frac{\pi d_p^3}{6} \Delta G_v}_{\text{volume energy}}$$

where $\Delta G_v = \frac{kT}{v_m} \ln S$
 v_m : molecular mass

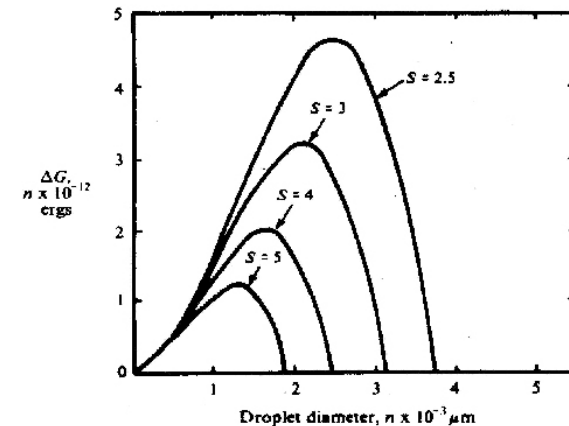
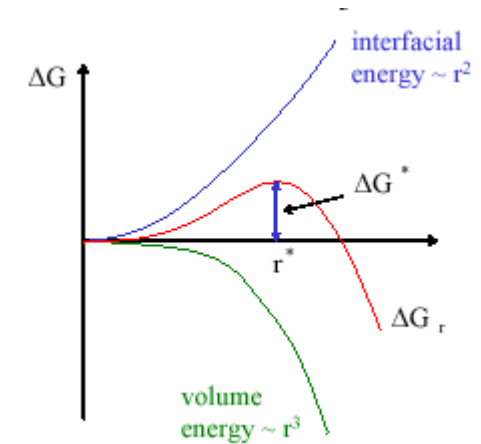
- Saturation ratio

For solution-to-particle: $S = \frac{c}{c_0}$

For vapor-to-droplet or particle: $S = \frac{p}{p_0}$

where c_0, p_0 : equilibrium solubility, vapor pressure

Gibbs free energy change for water droplet formation



- Critical nuclei

From $\frac{d\Delta G}{dd_p} = 0$

$$d_p^* = -\frac{4\sigma}{\Delta G_v} = \frac{4\sigma v_m}{kT \ln \frac{P}{P_0}}$$

Critical nuclei diameter

Kelvin equation

$$\Delta G^* = \frac{16\pi\sigma}{(3\Delta G_v)^2}$$

Energy barrier for nucleation

- Rate of nucleation

$J(\text{nuclei}/(\text{s})(\text{cm}^3)) = (\text{frequency of collision}) (\text{species concentration}) (\text{probability})$

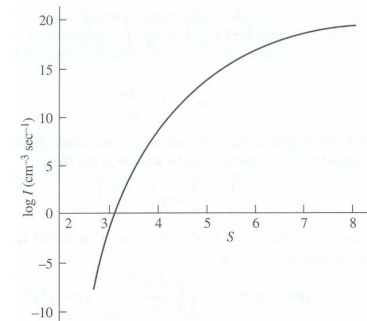
Solution-to-particle $J = \frac{kT}{3\pi d \mu} n_m \exp\left(-\frac{\Delta G^*}{kT}\right)$

Vapor-to-droplet or particle $J = \frac{P}{(2\pi mkT)^{1/2}} (\pi d_p^*)^2 n_m \exp\left(-\frac{\Delta G^*}{kT}\right)$

n_m : number concentration of the species

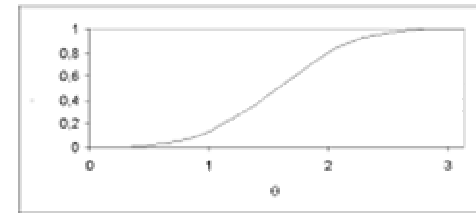
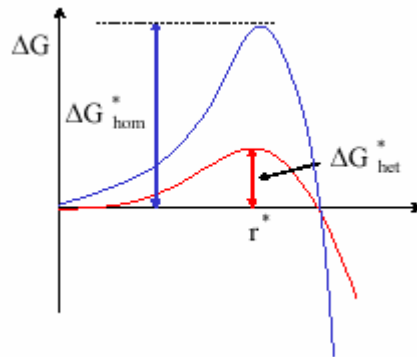
- Critical saturation, S_{crit}^* : S at $J=1$

Nucleation rate of water droplets at 300K



(2) *Heterogeneous nucleation*

$$\Delta G_{het}^* = f\Delta G^* = \frac{(2 + \cos \theta)(1 - \cos \theta)^2}{4} \Delta G^*$$



Correction term f vs. the contact angle in radian

* *Critical supersaturation ratio (S_{crit})*

If $S > S_{crit} \Rightarrow$ Homogeneous nucleation

$S < S_{crit} \Rightarrow$ Heterogeneous nucleation

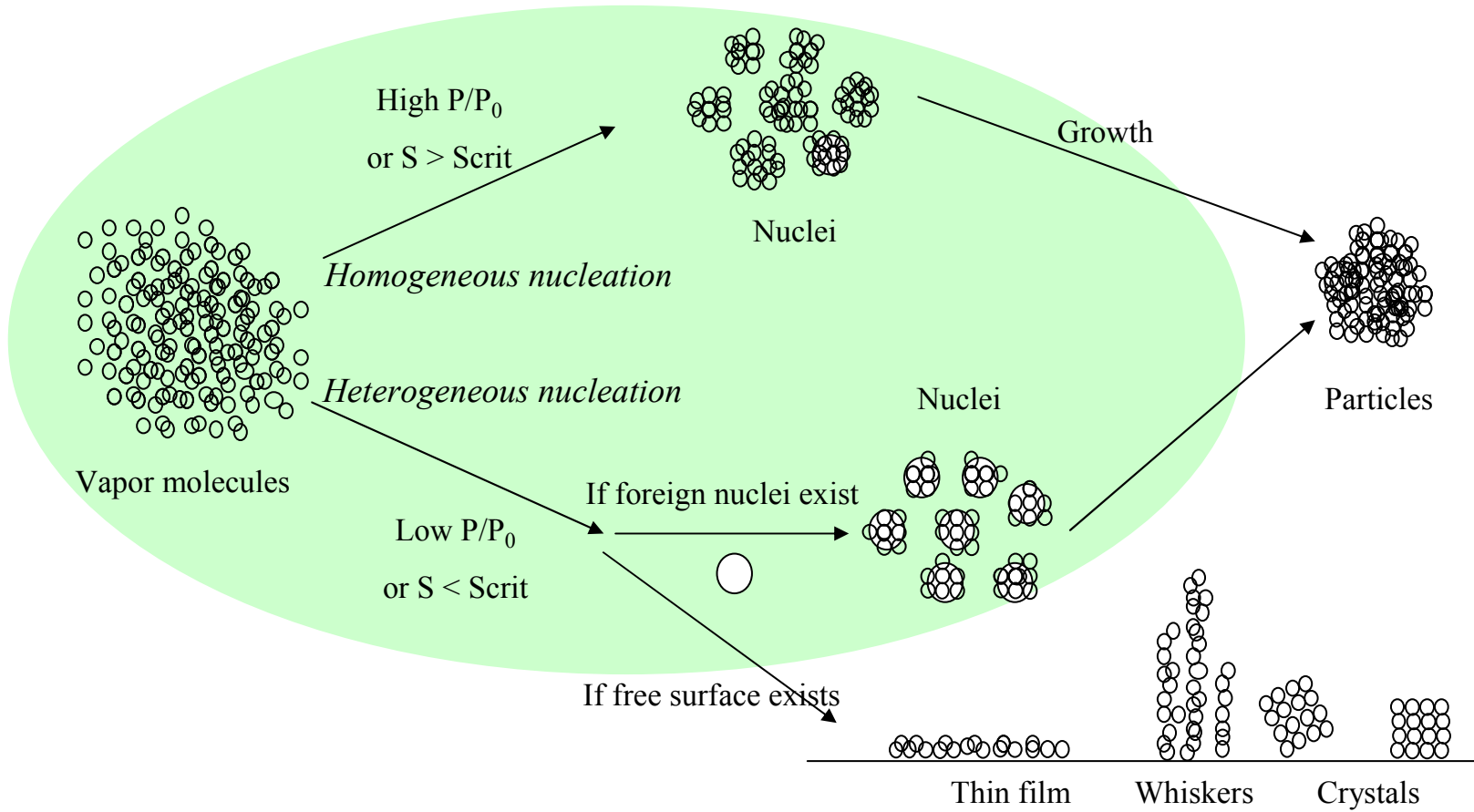
* *Used for formation of artificial rain (seed: AgCl, AgI)*

Core-shell particles

Monodisperse particles

Films

** Particles or Films?*



4.3 Condensational Growth of Nanoparticles



Growth of particles by collision followed by sticking

- Rate of condensation

<http://www.eng.uc.edu/~gbeaucag/Classes/Nanopowders/>

	Gas phase	Liquid phase
<i>Diffusion limited</i>	$d_p \ll \lambda_{gas} \quad \frac{dd_p}{dt} = \frac{2v_m(p_1 - p_2)}{(2\pi mkT)^{1/2}}$ $d_p \gg \lambda_{gas} \quad \frac{dd_p}{dt} = \frac{4Dv_m(p_1 - p_2)}{d_p kT}$	$\frac{dd_p}{dt} = \frac{4Dv_m(n_1 - n_2)}{d_p}$
<i>Surface reaction limited</i>	$\frac{dd_p}{dt} = \frac{2k_r \alpha v_m p_1}{(2\pi mkT)^{1/2}}$	$\frac{dd_p}{dt} = 2k_r v_m n_1$
<i>Droplet phase reaction limited</i>	$\frac{dd_p}{dt} = \frac{d_p}{3} \rho_p \left(\sum_{i=1}^R M_i v_i \right) r$	

If $p_1 < p_2$, evaporation instead of condensation

For diffusion-controlled condensation

Integration yields

$$d_p^2 = k_D t + d_{p0}^2 \quad (*) \quad \text{where} \quad k_D = 8Dv_m(n_1 - n_2)$$

Considering a variation in size $d_p = \langle d_p \rangle + \delta d_p$ and $d_{p0} = \langle d_{p0} \rangle + \delta d_{p0}$

Substituting these into (*), omitting square term which is small

$$\langle d_p \rangle^2 + 2 \langle d_p \rangle \delta d_p = k_D t + \langle d_{p0} \rangle^2 + 2 \langle d_{p0} \rangle \delta d_{p0}$$

Since $\langle d_p \rangle^2 = k_D t + \langle d_{p0} \rangle^2 \quad (**)$

Then
$$\delta d_p = \frac{d_{p0} \delta d_{p0}}{d_p}$$

Substituting (**)
$$\delta d_p = \frac{d_{p0} \delta d_{p0}}{\sqrt{k_D t + d_{p0}^2}}$$

The variation in size decreases as growth proceeds!

For surface reaction-controlled condensation

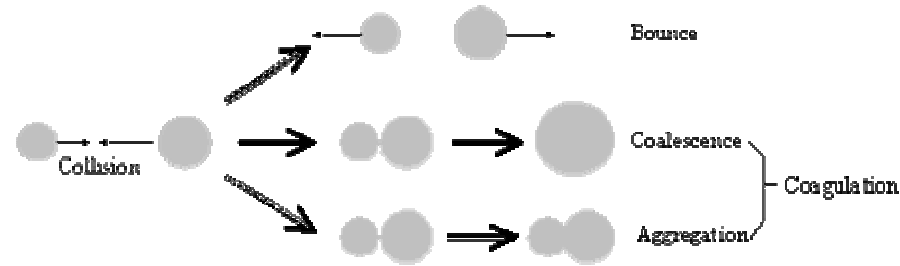
Integration $d_p = k_p t + d_{p0}$ where $k_p = 2k_r v_m n_1$

$$\therefore \delta d_p = \delta d_{p0}$$

The variation in size is kept constant but the relative size variation decrease as growth proceeds!

4.4 Coagulation: Coalescence and Aggregation

Growth as a result of collision and subsequent coagulation with other particles.



- Sources of collision

Brownian motion, external force fields, particle-particle interaction
(polar, coulombic)

- Coagulation efficiency

Comparison of condensation and coagulation

	<i>condensation</i>	<i>coagulation</i>
<i>size</i>	<i>increase</i>	<i>increase</i>
<i>Particle number concentration</i>	<i>No change</i>	<i>decrease</i>
<i>Total particle mass concentration</i>	<i>increase</i>	<i>decrease</i>

(1) *Shapes of particles coagulated (secondary particles)*

Spherical/near-spherical growth

: Liquid-phase or liquid-like growth

- Liquid particles grow by "coalescence"..*
- Solid particles grow by "aggregation (agglomeration)" and followed by rapid sintering*



Random (fractal) growth

: Solid-phase growth

- Fractal representation*

$$V \sim l^D$$






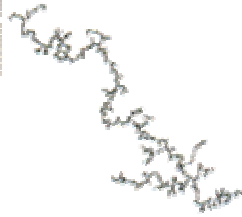
where V : solid volume

l : characteristic length of the aggregate

D : fractal dimension ($\neq 1, 2, 3$)



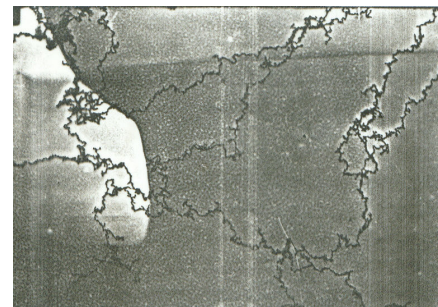
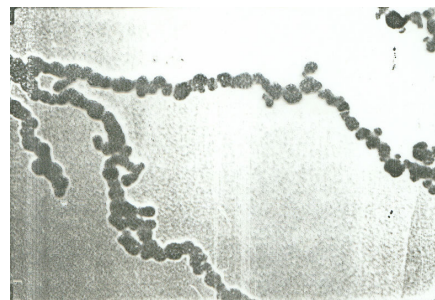
Aggregate of TiO₂ nanoparticles

	Reaction-limited	Ballistic	Diffusion-limited
Particle-cluster	 $D_f = 3.00$	 $D_f = 3.00$	 $D_f = 2.50$
Cluster-cluster	 $D_f = 2.09$	 $D_f = 1.95$	 $D_f = 1.80$

Directional (anisotropic) growth

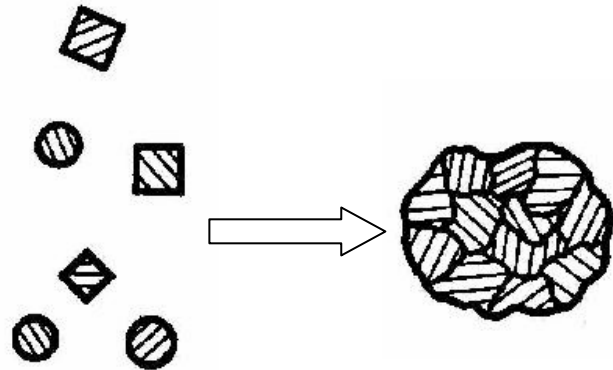
With interparticle forces - electrical or magnetic dipoles

e.g. Smoke particles, iron nanoparticles



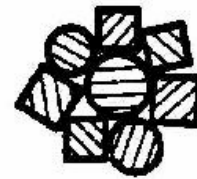
Iron particles

** Solid particle growth*



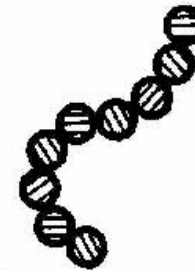
Fast sintering

Primary particles

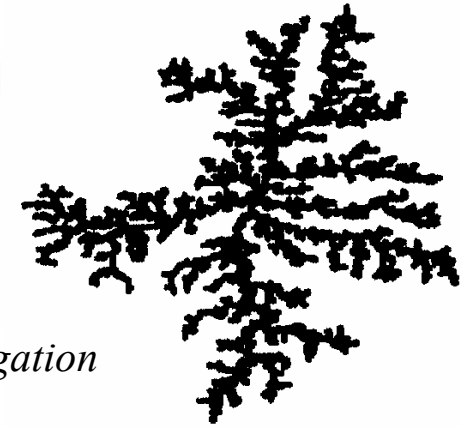


Slow sintering

Secondary particles



Dipole aggregation



Fractal growth

- Coalescence or Aggregation?

- Depends on the characteristic times of collision and coalescence

(2) Mathematical expression for coagulation

$N_{i,j}$: Number of collisions occurring per unit time per unit volume between the particles having diameters (volumes) $d_i(v_i)$ and $d_j(v_j)$ respectively.

$$N_{i,j} = b_{i,j} n_i n_j$$

n_i, n_j : number concentration of colliding particles v_i, v_j respectively. (no./cm³)

i, j : number of basic units making particles (e.g. i -mer and j -mer)

In terms of continuous size distribution

$$N(v_i, v_j) = b(v_i, v_j) n(v_i) n(v_j) dv_i dv_j$$

where $b_{i,j}$: collision frequency function

"coagulation coefficient"

Increase in size

$$v_{new} = v_i + v_j$$
$$d_{p,new} = \left(d_{pi}^3 + d_{pj}^3 \right)^{1/3}$$

- Change in number concentration of the particles, v

$$\frac{dn_k}{dt} = \frac{1}{2} \sum_{i+j=k} N_{i,j} - \sum_{i=0}^{\infty} N_{i,k} = \frac{1}{2} \sum_{i+j=k} b_{i,j} n_i n_j - n_k \sum_{i=0}^{\infty} b_{i,k} n_i$$

$$\frac{dn(v)}{dt} = \frac{1}{2} \int_0^v b(v', v-v') n(v') n(v-v') dv' - n(v) \int_0^{\infty} b(v, v') n(v') dv'$$

Input by coagulation Output by coagulation

- For Brownian coagulation

For continuum regime

$$b(v, v') = \left(\frac{2kT}{3\mu} \right) \left(\frac{1}{v^{1/3}} + \frac{1}{v'^{1/3}} \right) \left(v^{1/3} + v'^{1/3} \right) \quad \text{or}$$

$$b(v, v') = \left(\frac{2kT}{3\mu} \right) \left(\frac{1}{d_{pi}} + \frac{1}{d_{pj}} \right) (d_{pi} + d_{pj})$$

- For polydisperse particles

When $d_i > d_j$ $b_{i,j} > b_{i,i}$ or $b_{j,j}$

- Different-size coagulation occurs faster than that between similar-size coagulation.

Monodisperse particles becomes polydisperse...

Polydisperse particles becomes monodisperse...

∴ Self preserving model: distribution converges to $\sigma_g = 1.4$

- For monodisperse particles

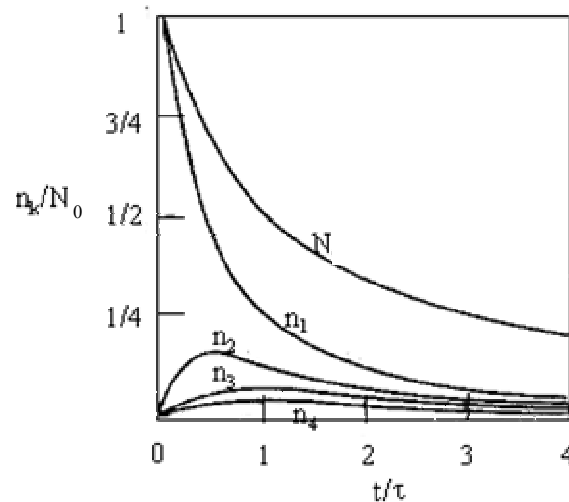
$$b = \frac{8kT}{3\mu} = K = 3.0 \times 10^{-16} C_c m^3 / s$$

Under standard conditions

$$\frac{dn_k}{dt} = \frac{K}{2} \sum_{i+j=k} n_i n_j - K n_k \sum_{i=0}^{\infty} n_i$$

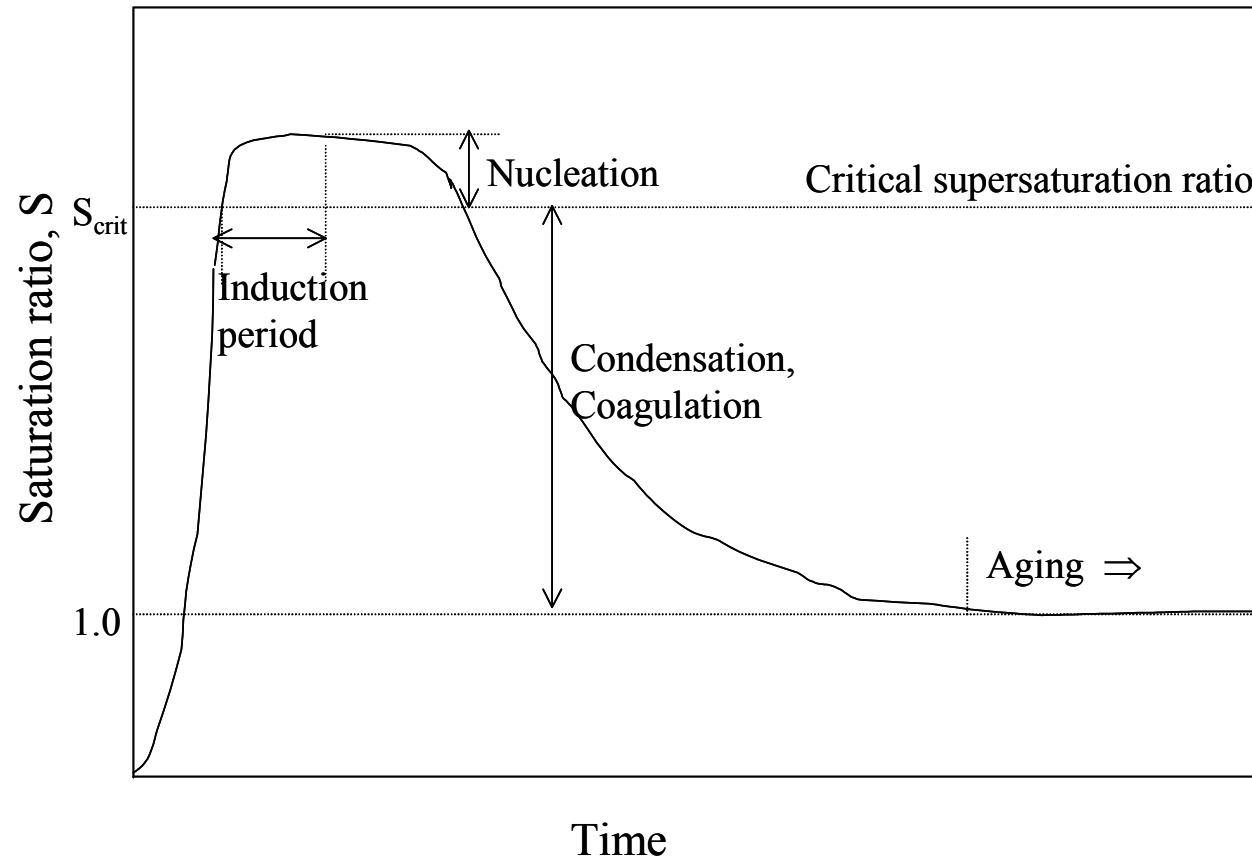
Solving for total number concentration of particles, N and average diameter of the particles, d

$$N(t) = \frac{N_0}{1 + N_0 K t} \quad \text{and} \quad \frac{d(t)}{d_0} = \left(\frac{N_0}{N(t)} \right)^{1/3}$$



4.5 Some Comments on Particle Growth

(1) Overall growth



(2) Growth mechanisms and particle size distribution

** Nucleation*

- increase of particle number concentration*
- may cause accelerating the rate of coagulation*
- gives delta function in particle size distribution in given condition*

** Condensation*

- No effect of particle number concentration*
- results in monodisperse size distribution.*

** Coagulation*

- Decreases in particle number concentration*
- gives polydisperse size distribution in growth process*

- Matijevic's method

(3) Preparation of monodisperse particles

- *Maintain low rate of nucleation*
 - *using low supersaturation*
 - *inducing heterogeneous nucleation*
- *Allow the same growth time for all the particles by shortening the time of nucleation*
- *Suppress coagulation*
 - *Using electrostatic repulsion (electrical double layer)*
 - *Using adsorption of surfactants and macromolecules*
 - *Rapid cooling and dilution*

(4) Composite particles

** Mixed –phase particles from mixtures of precursors:*

*Since reaction (or evaporation), critical supersaturation, saturation:
different for each component,*

- Different history of nucleation

- Possible occurrence of heterogeneous nucleation

- Different condensation rate

- uniform distribution of components within each particle: unexpected

“Composition gradient”

- Confined growth: preferred

e.g. spray-pyrolysis, emulsion, in-pore and in-layer growth

** Core-shell composite particles*

coating of existing particles

start with heterogeneous nucleation and subsequent growth