

Chapter 3.

- 80% polyethylene 가 (thermoplastic polymer)
- Ethylene 가 :
- (1) Low density PE (LDPE) -
- (2) High density PE(HDPE) -
- (3) Linear low density PE(LLDPE) -
- (4) Ethylene oligomer
- (5) Poly (vinyl chloride), (PVC)
- (6) Poly (vinyl acetate), (PVAc)
- (7) Polystyrene, (PS)
- (8) Poly (ethylene glycol), (PEG)

P. 101

3.1.2

- 1932 ICI . (200 1300-2600 bar)
- : 0.915 (g/cm³)
- .
- branched .
- 55% (T_m=110~120)
- organic peroxide



3.1.3

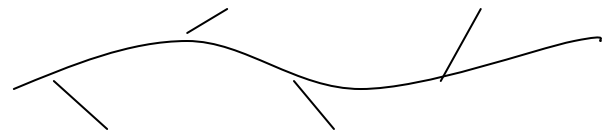
- 1954 Ziegler [$TiCl_4$ () / $Al(C_2H_5)_3$ ()]
- : 0.965 (g/cm³)
- blow molding linear
- 85~95% ($T_m=130\sim136$)



3.1.4

(LLDPE)

- LDPE HDPE
- 0.915 ~ 0.925 (g/cm³)
- Linear with short branch
- 55 ~60%
- comonomer 1-butene, 1-hexene or 1-octene
- LDPE . (Tensile strength)
- gauge films 가



3.1.5

polyethylene

- 가 0.941(g/cm³) PE ,

- rope .
- PE .
- Gel spinning (wax dichloromethane)
- , .

◆ Petrochemicals from ethylene.

. Ethylene

- 1990 , 125
- 1995 , 355
- 1995 () 2,200
- 2000 () 2,600

. Ethylene

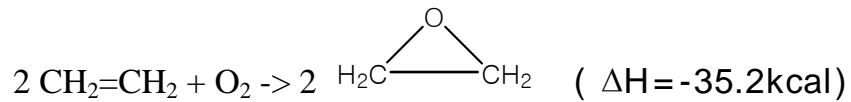
- readily available
- low cost
- high purity petrochemical industry prime raw material
- .

. Ethylene

- Polyethylene : 44%
- Ethylene oxide : 16%
- Vinyl chloride : 13%
- Ethyl benzene : 8%

- Others : 19%

(1) Ethylene Oxide (EO)

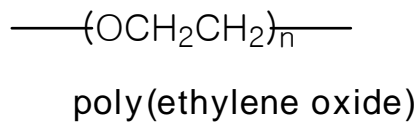
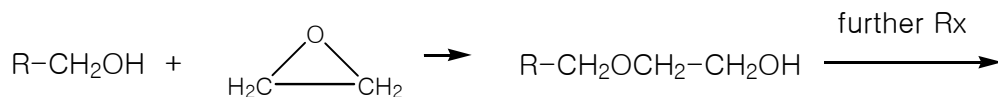


- Produced by air or O₂ oxidation.

- Silver

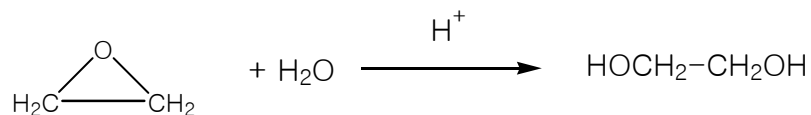
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- Poly(ethylene oxide) (PEO)

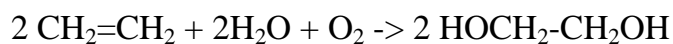


(2) Ethylene Glycol : CH₂OH-CH₂OH (EG)

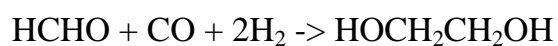
- (a) produced by hydration of ethylene oxide,



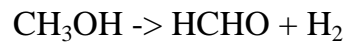
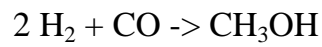
- (b) produced directly from ethylene, acetoxylation,



- (c) from formaldehyde and carbon monoxide

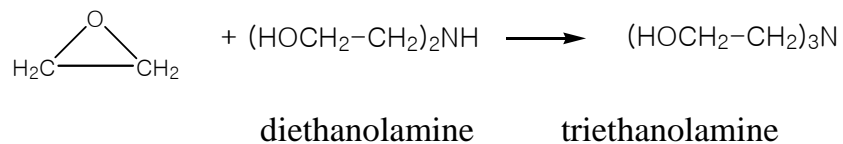
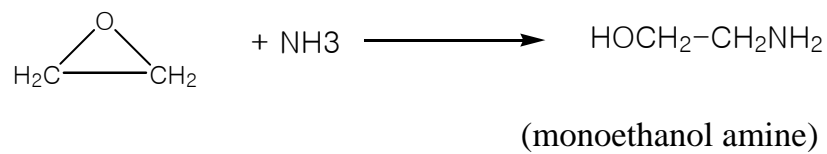


(d) from syn gas



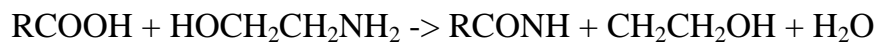
(3) Ethanolamine

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- sweetening of acid gases
- detergent()



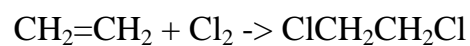
- for the production of ethanolamide detergents from fatty acids.

(4) Vinyl chloride, CH₂=CHCl

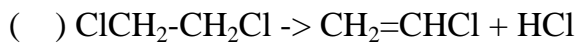
- 92% of the vinyl chloride monomer (VCM) is produced by the "balancedoxychlorination process".

()

() First step (direct chlorination) :

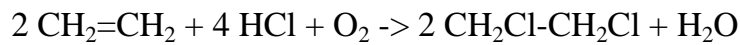


-to produce ethylene dichloride



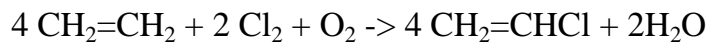
- second step is pyrolysis

() third step is oxychlorination,



recycled

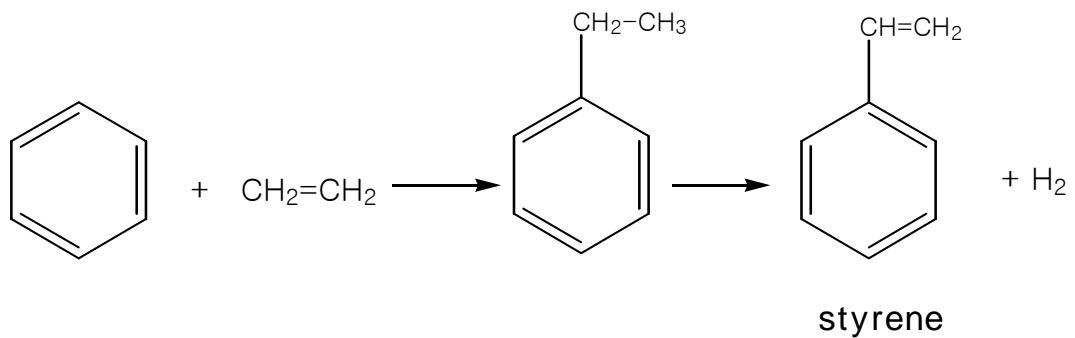
() overall reaction



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PVE – pipe, films, coatings, moldings

(5) Ethylbenzene



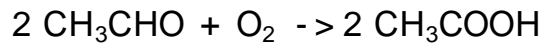
(6) Ethanol, ethyl alcohol, $\text{CH}_3\text{CH}_2\text{OH}$

()

() Fermentation is the process used.

() Synthetic process : indirect hydration of ethylene.

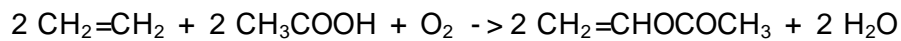
- by the liquid phase oxidation of acetaldehyde,



(8) Vinyl acetate :

- produced from ethylene and acetic acid

() gas phase



(most economical, .)

()

polyvinyl acetate , vinyl acetate copolymer, polyvinyl alcohol (more details in Chap. 12)

(9) Acrylic acid : $\text{CH}_2=\text{CHCOOH}$

- by oxidative carbonylation with carbon monoxide and oxygen with a palladium/copper

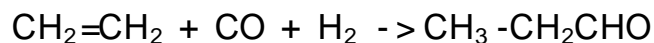


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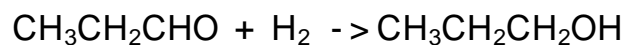
, plastics

(10) Propionaldehyde : $\text{CH}_3\text{CH}_2\text{CHO}$

- Produced by the hydroformylation of ethylene,



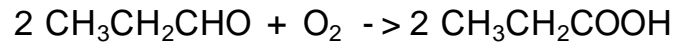
() () Propanol



- solvents for coatings .

- for ink used in painting on food containers.

() Propionic acid



- used as a

(11) Linear Alcohols :

- produced from ethylene from a four -step process

()

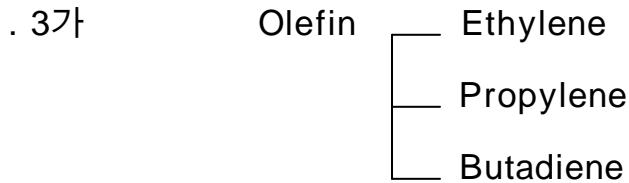
. C₁₂₋₁₆ range are used to make detergents.

C₁₀₋₁₂ : 가 (plasticizers)

C₁₆₋₁₈ : modifiers for was -and -wear resins.

C₂₀₋₂₆ : lubricants and mold -release agents.

Production of Olefins



Ethylene

- ethylene

4가 가

Naphtha (67%)

Gas oil (20%)

LPG (9%)

Ethane (4%)

(see Fig. 7.3)

. Gas oil - A liquid petroleum distillate with viscosity and boiling range between kerosine and lubricating oil. Boiling range between 230 and 430 .

Propylene - the second most important olefin.

- 63%가 ethylene coproduct

Butadiene - Olefin

- Ethylene coproduct

- Produced by butane and butene dehydrogenation.

() Olefin Feedstocks

- heavier feeds ethane

propylene, butadiene

BTX byproducts .

- Paraffin hydrocarbons, alkanes easiest to crack
- n -alkanes ethylene yield가 .
- Isobutane isopentene branched chain alkanes(isoparaffins) propylene yield가 .
- Naphthens cycloparaffins cracking 가 ,
the ring must be opened first.
- Ethane cracking 800
- Naphtha gas oil cracking 675~700 .

() Gas Feedstocks

- the gaseous feedstock for ethylene production

- () Ethane () Propane
- () n -Butane () various mixture of

these

() Ethane : High ethylene yield



Yield : wt%

Ethylene	80.9%
Hydrogen and Methane	12.9%
Propylene	1.8%
Butadiene	1.9%
Others	2.5%

. Ethane feedstock

Ethane 94.2%	Propylene 3.0 wt%
Acetylene 1.9 wt%	Propane 0.9 wt%

() Propane :

- Propane gives a lower ethylene yield and a longer quantity of coproduct

- Yield : wt% (see Table 7.1)

(a) Ethylene 44.0%

(b) Propylene 15.6%

(c) Butadiene 3.4%

(d) BTX 2.8

(e) Others 34.2

() Ethanepropane mixture

- cocracking (see Table 7.3)

() n -Butane

- is a minor source of ethylene.

- n -butane is cracked at the highest conversion level because any unconverted butane will be contained in the C₄ products.

This makes recovery of the butadiene and butanes more difficult and expensive.

() Liquid Feedstocks

() Naphtha - gas feedstock coproducts

- Cracking severity ethylene, propylene, butadiene yield % 가 .

() Reformer Raffinate

- Produce relatively less ethylene and more propylene than virgin (straight run) naphtha.

. Raffinate - the portion of an oil that is not dissolved in solvent refining of lubricating oil.

() Gas Oil

- a liquid petroleum distillate with viscosity and boiling range between kerosene and lubricating oil. Boiling range between 230~430

- not as desirable as naphtha

(ethylene naphtha)

- naphtha density가 , a lower hydrogen content, a higher sulfur content aromatic compounds

() Crude oil

- ethylene, BTX acetylene yield naphtha gas oil cracking crude oil direct cracking .

- 2가 process가 ..

The crude oil is sprayed directly into 2,000

superheated steam inside the reactor.

Direct cracking by a fluidized bed reactor.

() Other processes

- ethylene, other olefins BTX
process

() Hydropyrolysis - a cracking process characterized by
operating in the presence of hydrogen
under pressure.

- -

- (a) absence of a catalyst
- (b) higher operating temp.
- (c) shorter processing time

- -

- (a) : 800~900
- (b) : none
- (c) : 10~30 atm
- (d) : less than 0.1 sec

- Yield

. Vary with feedstock and recycling

- Feed stock Naphtha

- (a) Ethylene 44~45%
- (b) Methane 34%

(c) Aromatic gasoline 20%

- Feedstock gas oil

(a) Ethylene 35%

(b) Methane 25~30%

(c) Heavy fuel 13%

() Millisecond pyrolysis

- Millisecond furnace olefin pyrolysis

breakthrough가 가

- : 0.03~0.1s

- : 870 (moderate severity)

925 (high severity)

- ethylene yield가 10~20% 가

() Thermal Regenerative Cracking (TRC)

- a new process : Cost 20% feedstock

ethylene

() Cracking oil by steam and molton salts (COSMOS)

- cosmos process naphtha cracking

externally heated tubular furnace .

() Coproduct Treatment

- Ethylene demand governs the amount of coproduct
propylene, butadiene and BTX

- Heavier feedstocks will increase C4 production.

. Acetylene ($\text{HC}\equiv\text{CH}$)

- ethylene coproduct .

. Other source of ethylene

() Diolefin Butadiene Isoprene

() Butadiene - $(\text{CH}_2=\text{CH}-\text{CH}=\text{CH}_2)$

- raw material for the most widely used synthetic rubber.

- SBR(styrenebutadiene -rubber)

- polybutadiene

- Butadiene ethylene by-product

.
- the dehydrogenation of butane to butenes to butadiene is currently the most important "on purpose" source of butadiene.

()

$\text{CH}_3-\text{CH}_2-\text{CH}_2-\text{CH}_3 \rightarrow$ mixture of butanes $\rightarrow \text{CH}_3=\text{CH}-\text{CHCH}_3$

() Other methods for the production of butadiene.

(a) From ethyl alcohol

(b) The hydration of acetylene

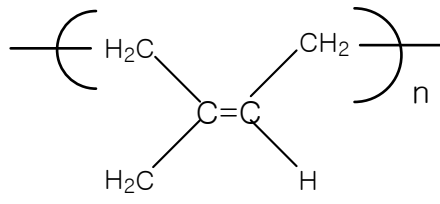
(c) from acetylene and formaldehyde

() Isoprene

$\text{CH}_2=\text{C}-\text{CH}=\text{CH}_2$, 2-methyl1,3-butadiene

- an important elastomer raw material

- cis-polyisoprene is similar in its structure to natural rubber.



cis -1,4 -polyisoprene

- isoprene cis -polyisoprene .