

## Chap. 30. Convective Mass Transfer Correlation

→ Rate of Mass Transfer(중요한 요인)

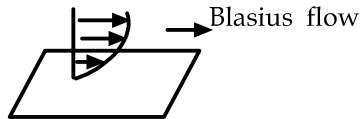


$$\text{Flux } N_A = k_c \Delta C_A$$

$$\Delta C_A = (C_{cause} - C_{Result})$$

$$\rightarrow Sh = \frac{k_c D}{D_{AB}} = f(Re, Sc)$$

theoretical approval



→ 다양한 계 (R,C,S)



empirical relation !



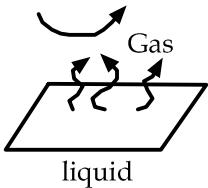
Grouping → Sherwood number

correlation → 상관관계  
(경험식)

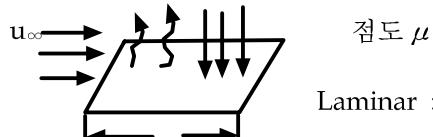
### 1. Mass transfer to plates, cylinder, spheres

between moving fluid & certain shape → vaporization &

dissolution of solid/sublimation of solid



#### (1) Flat plate



점도  $\mu$

$$\text{Laminar : } Sh_L = 0.664 Re^{\frac{1}{2}} Sc^{\frac{1}{3}}$$

$$\text{Turbulent : } Sh_L = 0.036 Re^{0.8} Sc^{\frac{1}{3}}$$

$$*\text{ j-factor : } j_b = \frac{Sh_L}{Re_L Sc^{\frac{1}{3}}}$$

$$(2) \text{ Single Sphere : } Sh = Sh_o + CR e^m Sc^{\frac{1}{3}}$$

↓      ↑ forced convection

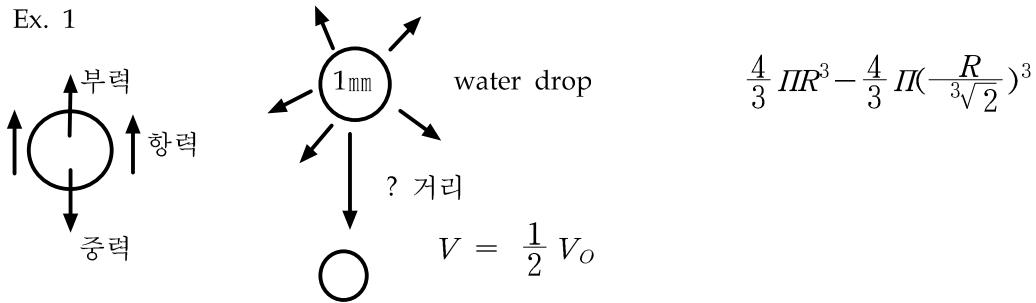
molecular diffusion =  $Sh_o = 2$

$$Sh = (4 + 1.21 Re^{\frac{2}{3}})^{\frac{1}{2}} : \text{Brian \& Hales (Pe = ReP_L)}$$

$$*\text{ Sh} = 2 + 0.552 Re^{\frac{1}{2}} Sc^{\frac{1}{3}} : \text{forced convection}$$

$$*\text{ Sh} = 2 + 0.57(GrSc)^{0.25} : \text{natural convection}$$

Ex. 1



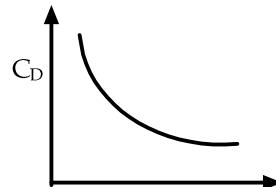
$$\frac{4}{3} \pi R^3 - \frac{4}{3} \pi \left(\frac{R}{\sqrt[3]{2}}\right)^3$$

$$\frac{1}{2} \times \frac{4}{3} \pi R^3 = \frac{1}{2} \frac{4}{3} \pi R_1^3 \quad R_1 = \frac{1}{\sqrt[3]{2}} R$$

Terminal velocity  $V_o = \sqrt{\frac{4dp(\rho_p - \rho)g}{3C_D\rho}}$

$$C_D = C_D(R_o) = C_D(V_o)$$

$$V_o = \sqrt{\frac{10.22}{C_D}}$$



$$C_D \text{ 가정} \rightarrow V_o$$

$$C_D = \text{결정} \quad V_o \rightarrow Re$$

$$\frac{\text{소멸된양}}{W_A} = t \quad t \times V_o = \text{거리}$$

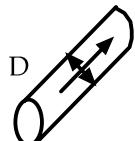
### (3) Single Cylinder



$$\frac{k_G P S c^{0.56}}{G_M} = 0.281 (Re)^{-0.4} \quad k_G = 1.34 \times 10^{-3} \text{ lb mole/hr ft}^2 \text{ mm}$$

## 2. Turbulent flow through a pipe

$$2000 < Re < 35000$$



$$\frac{k_c D}{D_{AB}} \frac{P_{b,lm}}{P} = 0.023 Re^{0.83} Sc^{0.44}$$

$$\downarrow$$

$$Sh = \frac{k_{Ld}}{D_{AB}} = 0.023 Re^{0.83} Sc^{\frac{1}{3}} \quad (k_L \Delta C_A \text{ or } k_G \Delta P)$$

$$\text{Area} : \pi D L \times N_A = W_A \frac{\text{물질질량}}{\text{시간}}$$