

Steam CO<sub>2</sub> reforming of methane over La<sub>1-x</sub>Sr<sub>x</sub>NiO<sub>3</sub> perovskite catalysts양은혁<sup>1,2</sup>, 노영수<sup>2</sup>, 정재선<sup>2</sup>, 홍기훈<sup>2</sup>, 키쇼<sup>2</sup>, 문동주<sup>2,†</sup><sup>1</sup>UST; <sup>2</sup>KIST

La<sub>1-x</sub>Sr<sub>x</sub>NiO<sub>3</sub> perovskite catalysts were prepared by EDTA-cellulose method and characterized by TPR, N<sub>2</sub> physisorption, TGA, XRD, TEM and SEM. The effect of promoting a perovskite (LaNiO<sub>3</sub>) catalyst with different amounts of Sr (0.1 - 0.5) to produce syngas via steam CO<sub>2</sub> reforming of methane was investigated. Steam CO<sub>2</sub> reforming of methane over the prepared catalysts carried out in a fixed bed reactor system under 900 °C, 10 bar and GHSV of 3000h<sup>-1</sup>. It was found that the 0.1 mole Sr-promoted catalyst had higher conversion and showed higher performance in terms of resisting deactivation by coke formation. It was found that the effect of Sr on activity, selectivity and stability are driven by segregated phases generated by Sr due to the difference of ionic radius between La and Sr. The Sr substituted perovskite had high O<sub>2</sub> mobility which led to higher gasification rates of carbonaceous species, resulting in higher H<sub>2</sub> generation and preventing carbon formation of the catalyst. Time on stream studies showed that La<sub>0.9</sub>Sr<sub>0.1</sub>NiO<sub>3</sub> is a potential candidate for steam CO<sub>2</sub> reforming of methane to produce syngas.