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Convective Instability in Horizontal Fluid Layers Heated with Constant Heat Flux

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1296 가 가 가 Rayleigh 가
 가 . 가 가
 , t_c 가 . Morton[1]
 , Foster[2]
 . Yang Choi[3] t_c
 . Nielsen Sabersky[4] 가
 . Malher
 [5] 가
 가

가 d T_i
 q_w 가 Rayleigh-Bénard ,
 Fig. 1 T_i ,
 가 가 가 가
 . Boussinesq 가 2 가

$$\frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0 \tag{1}$$

$$\frac{\partial v}{\partial \tau} + v \frac{\partial v}{\partial y} + w \frac{\partial v}{\partial z} = -\frac{\partial p}{\partial y} + Pr \left[\frac{\partial^2 v}{\partial y^2} + \frac{\partial^2 v}{\partial z^2} \right] \tag{2}$$

$$\frac{\partial w}{\partial \tau} + v \frac{\partial w}{\partial y} + w \frac{\partial w}{\partial z} = -\frac{\partial p}{\partial z} + Pr \left[\frac{\partial^2 w}{\partial y^2} + \frac{\partial^2 w}{\partial z^2} \right] + Pr Ra_q \theta \tag{3}$$

$$\frac{\partial \theta}{\partial \tau} + v \frac{\partial \theta}{\partial y} + w \frac{\partial \theta}{\partial z} = \frac{\partial^2 \theta}{\partial y^2} + \frac{\partial^2 \theta}{\partial z^2} \tag{4}$$

v, w , α/d ,
 k $\theta(=k(T-T_i)/q_w d)$. y, z ,
 d , $p(=Pd^2/\rho\alpha^2)$ P , $\tau(=\alpha/d^2)$ t
 Prandtl $Pr(=v/\alpha)$ Rayleigh
 $Ra_q(=g\beta q_w d^4/k\alpha v)$, v , β ,
 가 g Rayleigh .

$$\theta = 0 \quad \text{at } \tau = 0 \text{ and } z = 1 \quad (5)$$

$$\partial\theta/\partial z = -1 \quad \text{at } z = 0 \quad (6)$$

가 , 가 (5), (6) 가

$$\theta_0 = 2\sqrt{\tau} \sum_{n=0}^{\infty} (-1)^n \left\{ \text{ierfc}\left(\frac{n}{\sqrt{\tau}} + \frac{\zeta}{2}\right) - \text{ierfc}\left(\frac{n+1}{\sqrt{\tau}} - \frac{\zeta}{2}\right) \right\} \quad (7)$$

$$\theta_0 = k(T_0 - T_i)/q_w d, \quad \zeta = z/\sqrt{\tau}$$

$$\theta_1 = Ra_q(\theta - \theta_0)$$

[3]. $[w_1(\tau, y, z), \theta_1(\tau, y, z)] = [\tau^{3/2} w^*(\zeta), \tau^{1/2} \theta^*(\zeta)] \exp[i(ay)]$ (8)

i , a [3].

$$\left\{ (D^2 - a^{*2})^2 + \frac{1}{2Pr} (\zeta D^3 - a^{*2} \zeta D + 3a^{*2}) \right\} w^* = a^{*2} \theta^* \quad (9)$$

$$\left\{ D^2 + \frac{1}{2} \zeta D - \left(a^{*2} + \frac{1}{2} \right) \right\} \theta^* = Ra_q^* w^* D \theta_0^* \quad (10)$$

$$a^* = a\tau^{1/2}, \quad Ra_q^* = Ra_q \tau^2, \quad D = d/d\zeta, \quad D\theta_0^* = \tau^{-1/2} D\theta_0$$

$$w^* = Dw^* = D\theta^* = 0 \quad \text{at } \zeta = 0 \quad (11)$$

$$w^* = Dw^* = \theta^* = 0 \quad \text{at } \zeta = 1/\sqrt{\tau} \quad (12)$$

“shooting method”

가 . Mahler

[5] Foster[6] Patankar[7]

(1)~(6) 2 SIMPLE

가 $\Delta\tau = 10^{-7}$ $\Delta z = 1/200$

$$w(\tau, z)|_{\tau=0} = w_*(w_1(\tau, z)/w_{1,\max})|_{\tau=\tau_c} \quad (13)$$

$$\theta'(\tau, z)|_{\tau=0} = \theta_*(\theta_1(\tau, z)/\theta_{1,\max})|_{\tau=\tau_c} \quad (14)$$

$$\tau_c \quad w_*/\theta_* = 10^3$$

$Pr \rightarrow \infty$ Ra_q τ_c Fig. 2 $3.2\tau_c$
Nielsen Sabersky[4] 가

$$\tau = 3.2\tau_c, \quad \tau = \tau_c$$

Fig. 3

Fig. 4

$$(w_{rms}, \theta'_{rms}) = \left(\left[\int_A w^2 dA \right]^{1/2}, \left[\int_A \theta'^2 dA \right]^{1/2} \right) / A \quad (15)$$

$$\theta = \langle \theta \rangle + \theta'$$

$$\langle \theta \rangle$$

가 τ 가

$$r_0 = \frac{1}{\langle \theta \rangle_{rms}} \frac{d\langle \theta \rangle_{rms}}{d\tau} \quad (16)$$

$$r_1 = \frac{1}{\theta'_{rms}} \frac{d\theta'_{rms}}{d\tau} \quad (17)$$

Fig. 5

(7)

Fig. 4

r_1 가

$$r_0 > r_1, \quad r_1 > 0$$

$$r_1 \geq r_0$$

$$r_1 > r_0 \text{ 가 } \tau_c \text{ 가}$$

$$Nu (= q_w d / (T_w - T_i)) \text{ 가}$$

Kim Kim[8] Nu 가 가

Fig. 6

Nu

$3.2\tau_c$

Nusselt
Fig. 6

$3.2\tau_c$

가 가

τ_c

BK21

LG

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2. Foster, T.D.: *Phys. Fluids*, **8**, 1249(1965)
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4. Nielsen, R.C. and Sabersky, R.H.: *Int. J. Heat Mass Transfer*, **16**, 2407(1973)
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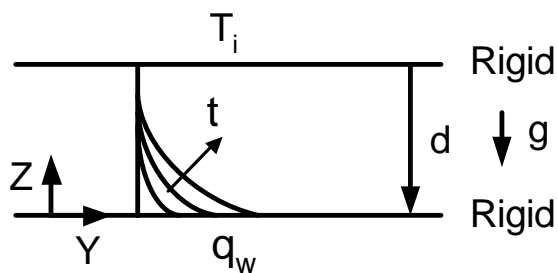


Fig. 1. Schematic diagram of the basic conduction state.

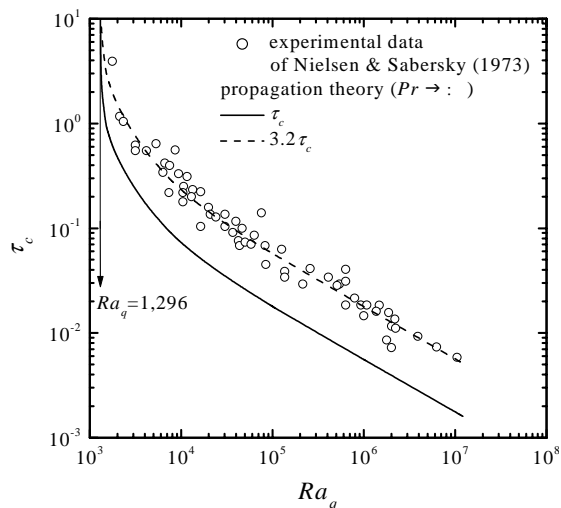


Fig. 2. Onset of convection.

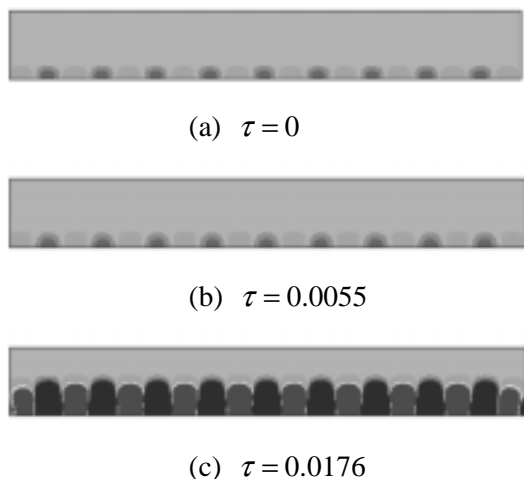


Fig. 3. Temperature disturbances.

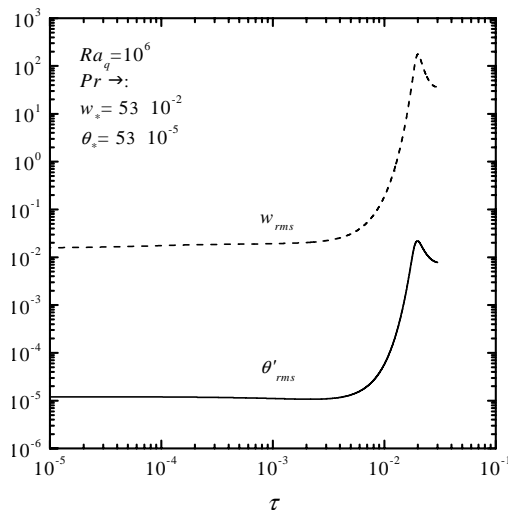


Fig. 4. Temporal behavior of disturbances.

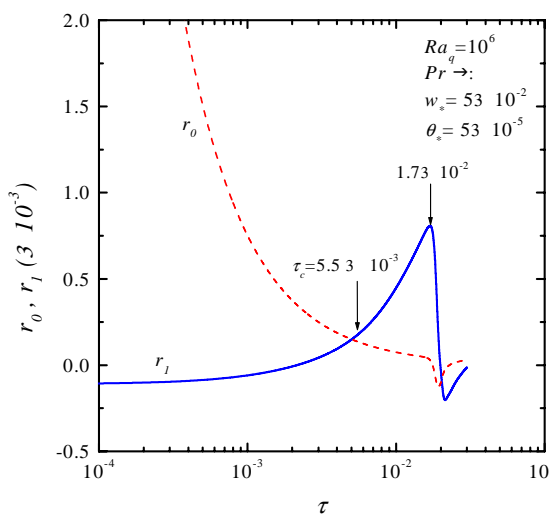


Fig. 5. Growth rate of temperature disturbances.

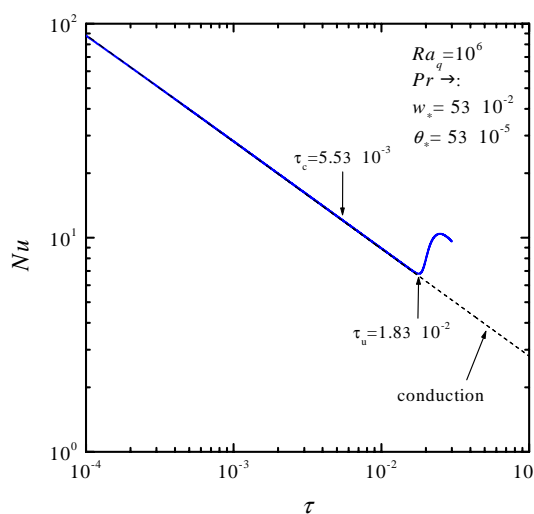


Fig. 6. Time-dependent Nusselt number.