An Electrolyte NLF - HB Equation of State Applicable to Concentrated Electrolyte systems

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Results

Conclusions

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Introduction

Electrolyte solutions

- Wastewater treatment, extraction, distillation, seawater desalination, salt-added bioseperation...
- Need for understanding of thermodynamics
- For engineering purposes
 - Experimental work
 - A good model capable of describing the phase behavior

Introduction

- More difficult to model than most other solutions
 - lons : Interaction both each other and with solvents
 - Charged particles
 - Low concentration : dominant electrostatic force
 - High concentration : Short-range forces become important.
 - The chemistry of solutions changes at different conditions such as temperature and density.

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Introduction

- Excess Gibbs function
 - Debye-Hückel, Pitzer model, electrolyte NRTL ...
 - Useful for non-idealities of electrolyte solutions
 - Not adequate to high pressure applications
- Equation of state approch
 - Applicable to wide range of pressure
 - Description of phase equilibria using unified model

- Development of an equation of state for electrolyte systems
 - Fully ionized electrolyte solutions
 - Electrostatic interactions => Mean spherical approximation(MSA) model
 - Association(or hydration) => Veytsman statistics

- Helmhlotz free energy
 - $A = A_{athm} + A_{res} + A_{ass} + A_{lr}$
 - Athermal contribution
 - Guggenheim Huggins Miller approximation
 - Residual contributions
 - Quasi-chemical approximation
 - Association contributions
 - Normalized Veytsmann statistics
 - Long-range contributions
 - Mean spherical approximation

Helmhlotz free energy

$$\begin{split} \beta A_{athm} &= -\ln N_r! + \sum \ln N_i! - \left(\frac{z}{2}\right) \left[N_q \ln N_q - N_{fq} - N_r \ln N_r + N_r \right] \\ \beta A_{res} &= -\left(\frac{z\beta N_q}{2}\right) \left[\sum \sum \theta_i \theta_j \varepsilon_{ij} + \left(\frac{\beta}{2}\right) \sum \sum \sum \theta_i \theta_j \theta_k \theta_l \varepsilon_{ij} (\varepsilon_{ij} + \varepsilon_{kl} - \varepsilon_{ik} - \varepsilon_{jk}) \right] \\ \beta A_{ass} &= N^{HB} \ln N_r - \sum_i^m (N^i_{\ d} \ln N^i_{\ d} - N^i_{\ d}) + \sum_i^m (N_{i0} \ln N_{i0} - N_{i0}) \\ &+ \sum_i^m \sum_j^n (\beta N_{ij}^{\ HB} A_{ij}^{\ HB} + N_{ij}^{\ HB} \ln N_{ij}^{\ HB} - N_{ij}^{\ HB}) \\ &- \sum_i^n (N^i_{\ a} \ln N^i_{\ a} - N^i_{\ a}) + \sum_j^m (N_{j0} \ln N_{j0} - N_{j0}) \\ \beta A_{lr} &= \frac{\Gamma^3 V}{3\pi} - \frac{\alpha^2}{4\pi} \sum_{ions} \left(\frac{N_k z_k^2 \Gamma}{1 + \Gamma \sigma_k}\right) \end{split}$$

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Chemical potential :

$$\frac{\mu_i}{RT} = \frac{\mu_i}{N_a kT} = \left(\frac{\partial \beta A^C}{\partial N_i}\right) + r_i v_H \beta P$$

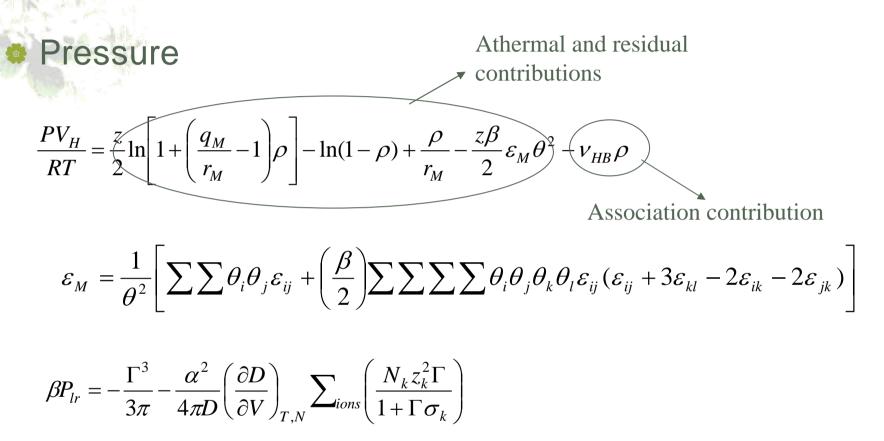
$$\beta \mu_i = (r_i + l_i) \ln \left[1 + \left(\frac{q_M}{r_M} - 1\right) \rho \right] - r_i \ln(1 - \rho) + \ln \left(\frac{\theta_i}{q_i}\right)$$

$$+\left(\frac{z\beta}{2}\right)q_{i}\varepsilon_{M}\theta^{2}\times\left[1-\frac{r_{i}}{q_{i}}-\frac{2\sum\theta_{k}\varepsilon_{ik}+\beta\sum\sum\theta_{j}\theta_{k}\theta_{l}\varepsilon_{ij}(\varepsilon_{ij}+2\varepsilon_{kl}-2\varepsilon_{jk}-\varepsilon_{ik})}{\varepsilon_{M}\theta^{2}}\right]$$

$$\beta \mu_{ass} = -\sum_i d_i^k \ln \frac{N_d^i}{N_{i0}} - \sum_j a_j^k \ln \frac{N_a^j}{N_{j0}}$$

$$\beta \mu_{i,lr} = -\frac{\alpha^2}{4\pi} \frac{z_i \Gamma}{(1 + \Gamma \sigma_i)} + \frac{\alpha^2}{4\pi D} \left(\frac{\partial D}{\partial N_i}\right)_{T,V,N_j} \sum_{ions} \left(\frac{z_k^2 \Gamma}{1 + \Gamma \sigma_k}\right)$$

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- Parameters for solvent
 - energy and size parameters

$$\varepsilon_{ii} / k = \varepsilon_a + \varepsilon_b (T - T_0) + \varepsilon_c [T \ln(T_0 / T) + (T - T_0)]$$

 $r_i = r_a + r_b (T - T_0) + r_c [T \ln(T_0 / T) + (T - T_0)]$

- Hydrogen bonding energy and number of donor and acceptor
- Obtained by fitting saturated vapor pressure and density

Three parameters for salts

- Interaction energy and segment number
 - Mean values of cation and anion

$$\varepsilon_{salt} = \varepsilon_{cation} = \varepsilon_{anion}$$
 and $r_{salt} = r_{cation} = r_{anion}$

• Size in MSA term

 $\sigma_i^3 = 6 f_c V_H r_i / \pi$

- Hydration energy and donor number for cations
 - Fixed to 7 for donor number
- Obtained by fitting mean activity coefficients and osmotic coefficients

Thermodynamic properties

Mean ionic chemical potential and mole fractions

$$\mu_{\pm i}(\nu_{+i} + \nu_{-i}) = \mu_{+i}\nu_{+i} + \mu_{-i}\nu_{-i} \qquad x_{\pm i}^{(\nu_{+i} + \nu_{-i})} = x_{+i}^{\nu_{+i}}x_{-i}^{\nu_{-i}}$$

Molal mean activity coefficient and osmotic coefficient

$$\ln \gamma_{\pm i}^{m^*} = \ln \gamma_{\pm i}^{l^*} - \ln \left(1 + \sum_{k=1}^{salt} \nu_{\pm k} x_k / \sum_{j=1}^{solvent} x_j \right)$$

where
$$\gamma_{\pm i}^{l^*} = \exp[(\mu_{\pm i}^l - \mu_{\pm i}^{l^\infty}) / RT] / x_{\pm i}^l \times x_{\pm i}^\infty$$

$$\phi = -x_S \ln x_S \gamma_S / RT \sum_{ions} x_k$$

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Parameters for salts

Salt	$arepsilon_{ii}$	r _i	Hydration energy	Salt	$arepsilon_{ii}$	r _i	Hydration energy
HCl	160.625	1.13	1887	NaI	90.828	2.05	1650
HBr	90.711	3.67	1890	$NaClO_4$	66.075	3.22	1770
Ш	120.453	2.65	1900	$NaNO_3$	47.111	2.29	1620
HClO ₄	175.063	1.00	2270	NaOH	53.504	2.05	2100
HNO_3	74.686	4.23	2180	$NaClO_3$	62.809	3.36	1746
LiCl	117.406	1.05	1955	NaAc	79.484	3.70	1895
LiBr	129.781	1.16	2170	NaTol	69.260	4.64	1658
LiI	89.563	3.65	2290	NaF	52.414	2.49	1690
LiClO ₄	87.395	3.60	2380	$NaBrO_3$	39.049	2.25	1715
LiNO ₃	79.959	3.52	1800	Na formate	72.371	3.66	1760
LiOH	66.219	0.84	1260	Na propionate	85.461	3.70	1860
LiAc	71.973	2.87	1798	Na H molanate	47.152	2.18	1650
LiTol	70.379	4.68	1905	Na H succinate	46.344	2.20	1768
NaCl	247.250	1.26	1130	NaCNS	76.408	4.35	1905
NaBr	186.688	1.62	1160	NaH_2PO_4	7.232	1.55	1875

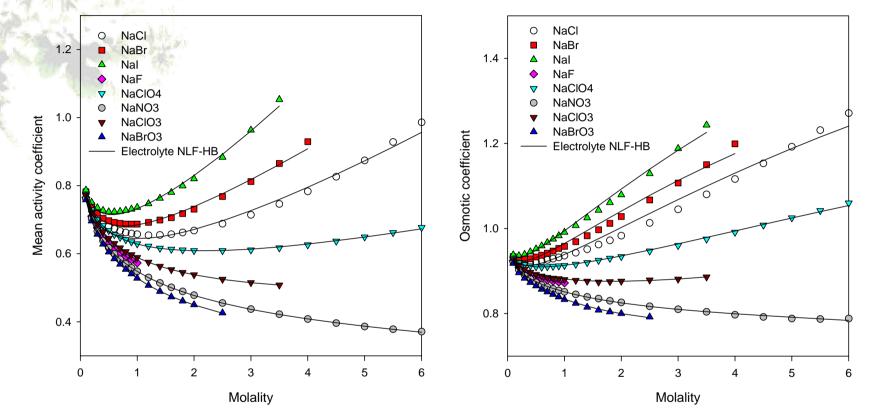
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Parameters for salts

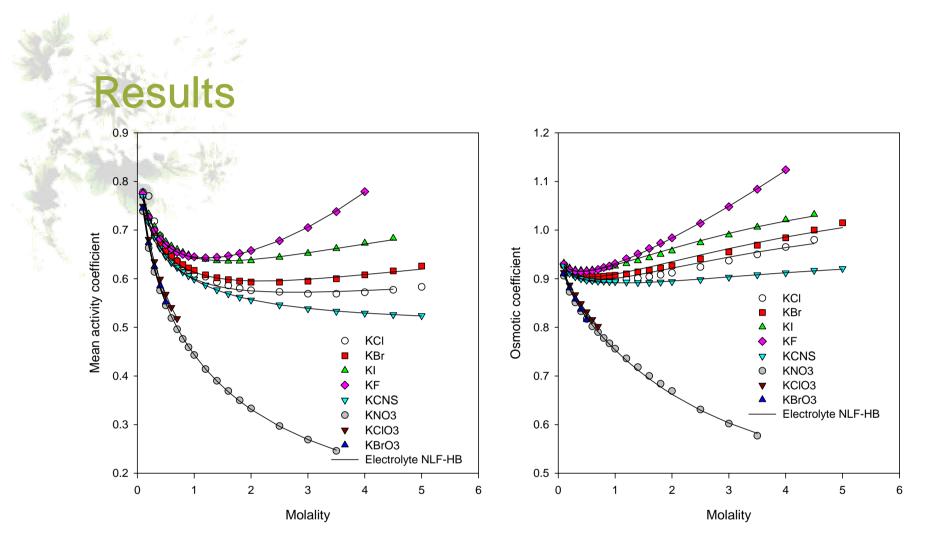
Salt	$arepsilon_{ii}$	r _i	Hydration energy	Salt	$arepsilon_{ii}$	r _i	Hydration energy
KCl	55.695	1.47	1500	RbCl	41.967	1.76	1680
KBr	59.129	1.78	1560	RbBr	41.967	1.76	1680
KI	70.719	2.32	1570	RbI	49.962	2.48	1792
KNO3	9.852	1.71	1750	RbNO ₃	0.777	1.32	1720
KOH	74.984	2.12	2070	RbAc	82.186	3.60	1950
KClO ₃	50.609	3.01	1440	CsCl	36.219	1.92	1755
KAc	82.133	3.59	1900	CsBr	36.406	2.20	1900
KTol	74.413	7.32	1796	CsI	42.031	2.65	2000
KF	57.582	2.50	1971	$CsNO_3$	0.122	1.32	1780
KBrO_3	45.688	3.44	1750	CsOH	86.211	2.84	1760
KH malonate	39.477	2.18	1665	CsAc	82.672	3.95	1966
KH succinate	41.873	2.28	1801	NH4Cl	57.910	2.32	1642
KH adipate	61.344	3.38	1965	$NH4NO_3$	58.484	3.72	1712
KCNS	60.342	2.60	1636	$AgNO_3$	0.0256	1.20	1663
$\mathrm{KH}_{2}\mathrm{PO}_{4}$	5.178	1.81	2848	TlAc	7.350	0.94	1503

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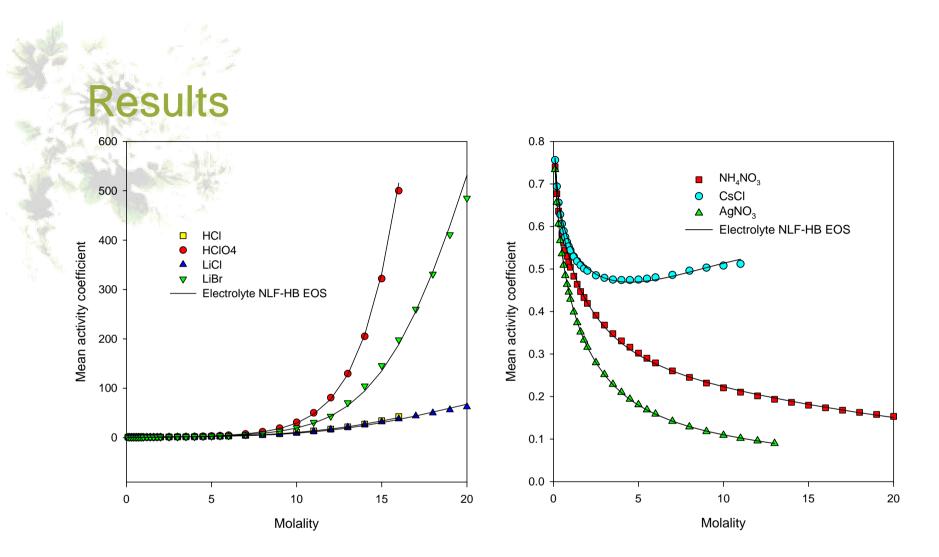
Results



Comparison of experimental mean activity coefficient and osmotic coefficient and calculated results



Comparison of experimental mean activity coefficient and osmotic coefficient and calculated results



Comparison of experimental mean activity coefficients and calculated results for concentrated electrolyte solutions

Comparison of Models

- Electrolyte NRTL model(based on G^E model)
 - Chen et al. (1999)
 - Two adjustable parameters and hydration number
- Myers and Sandler (2002)
 - Equation of state approach
 - Three adjustable parameters for each salts
 - The Born contribution for hydration process and MSA model for electrostatic interaction



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<u> </u>	E	Electrolyt	e NLF-H	В	NRTL	Sandler		Electrolyte NLF-HB			NRTL	Sandler	
	γ_{\pm}	ø	ρ	Max. molal	γ_{\pm}	γ_{\pm}		γ_{\pm}	ø	ρ	Max. molal	γ_{\pm}	γ_{\pm}
HCl	2.03	0.89	0.98	16.0	0.53	0.63	NaI	0.84	0.58	0.59	3.5	0.57	0.19
HBr	0.12	0.79	3.68	1.0	0.75	0.09	$NaClO_4$	0.21	0.15	3.54	6.0	0.46	0.07
HI	1.33	0.89	2.20	3.0	0.62	2.61	$NaNO_3$	0.13	0.15	3.29	6.0	0.12	0.11
HClO_4	2.94	1.28	10.70	16.0	1.19	0.20	NaOH	1.55	0.97	19.32	20.0	0.63	0.67
HNO ₃	0.09	0.13	6.64	3.0	0.80	0.06	$NaClO_3$	0.08	0.11	4.38	3.5	0.30	0.09
LiCl	3.56	1.53	0.18	20.0	0.88	0.25	NaAc	0.13	0.12		3.5	0.79	0.61
LiBr	3.24	1.26	1.83	20.0	0.95	0.37	NaTol	0.49	0.55		4.0	0.99	0.44
LiI	1.35	0.97	4.55	3.0	1.78	1.29	NaF	0.03	0.02	4.13	1.0	0.02	0.02
LiClO ₄	0.88	0.57	4.14	4.0	1.32	4.26	$NaBrO_3$	0.12	0.12	0.82	2.5	0.10	0.08
LiNO ₃	0.29	0.16	7.24	13.0	0.35	1.55	Na formate	0.17	0.25		3.5	0.71	0.31
LiOH	0.46	0.47	4.19	4.0	3.00	1.01	Na propionate	0.15	0.13		3.0	1.01	0.76
LiAc	0.19	0.13		4.0	0.22	0.30	Na H molanate	0.20	0.16		5.0	0.36	0.26
LiTol	0.59	0.61		4.5	0.97	0.58	Na H succinate	0.16	0.15		5.0	0.35	0.20
NaCl	1.63	1.20	0.99	6.0	0.44	0.08	NaCNS	0.27	0.14	7.09	4.0	1.22	0.36
NaBr	0.93	0.70	1.04	4.0	0.36	0.09	NaH_2PO_4	0.32	0.40	1.20	6.0	0.27	0.30

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- 5	ti uname ke si sel Kija	Electrolyte NLF-HB			NRTL	Sandler		Electrolyte NLF-HB					Sandler	
		γ_{\pm}	ø	ρ	Max. molal	γ_{\pm}	γ_{\pm}		γ_{\pm}	ø	ρ	Max. molal	γ_{\pm}	γ_{\pm}
	KCl	0.71	0.56	0.20	4.8	0.23	0.08	RbCl	0.07	0.07	0.33	5.0	0.15	0.07
	KBr	0.58	0.41	0.30	5.0		0.09	RbBr	0.12	0.09	0.33	5.0	0.16	0.07
	KI	0.44	0.27	0.25	4.5	0.38	0.20	RbI	0.52	0.37	0.50	5.0	0.18	0.12
	KNO_3	0.44	0.49	0.95	3.5	0.58	0.13	RbNO ₃	0.59	0.59	2.99	4.5	0.85	0.19
	KOH	1.12	0.47	12.35	16.0	0.48	0.60	RbAc	0.18	0.14		3.5	0.70	0.83
	KClO3	0.09	0.08	0.41	0.7	0.24	0.08	CsCl	1.39	1.01	1.48	11.0	0.52	0.28
	KAc	0.19	0.13		3.5	0.66	0.61	CsBr	1.05	0.82	0.95	5.0	0.52	0.31
	KTol	0.44	0.55		3.5	2.47	0.35	CsI	0.84	0.75	0.90	3.0	0.52	0.17
	KF	0.08	0.09	6.90	4.0	0.36	0.08	CsNO_3	0.50	0.50	1.55	1.4	0.24	0.15
	$KBrO_3$	0.08	0.11	0.61	0.5	0.14	0.08	CsOH	0.13	0.19	2.09	1.0		0.46
	KH malonate	0.47	0.49		5.0	0.36	0.52	CsAc	0.20	0.18		3.5	0.79	0.65
	KH succinate	0.19	0.17		4.5	0.21	0.22	NH4Cl	0.09	0.09	1.90	6.0	0.06	0.29
	KH adipate	0.10	0.06		1.0	0.12	0.09	NH ₄ NO ₃	1.62	1.56	10.32	20.0	0.93	0.16
	KCNS	0.12	0.12	0.08	5.0	0.13	0.13	AgNO ₃	0.41	0.57	0.94	13.0	0.77	0.20
	$\mathrm{KH}_{2}\mathrm{PO}_{4}$	0.61	0.43	0.78	1.8	0.22	0.08	TlAc	0.20	0.25		6.0	0.92	0.23

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Results : Summary

	E	lectrolyte NL	F	NRTL	Sandler		
Property	γ_{\pm}	φ	ρ	γ_{\pm}	γ_{\pm}		
AAD(%)	0.63(0.40 ª)	0.45(0.35 °a)	3.18(2.19ª)	0.61 ª	0.41 ª		

a : calculated up to 6 molal

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Conclusion

- Development of electrolyte NLF-HB equation of state
 - Electrostatic interactions by mean spherical approximation
 - Hydration(association) contribution by Veytsmann statistics
- Mean activity coefficients, osmotic coefficients, and densities were calculated for 60 electrolyte solutions