

*Innovation for Our Energy Future*

# Biomass Technologies: Overview and Future Trends

## Small Wood 2004

### Sacramento, CA

May 20, 2004

John Scahill

# Biomass Feedstocks



**Forest Wood Residues**

**Thinning Residues**  
**Wood chips**  
**Urban Wood waste**  
pallets  
crate discards  
wood yard trimmings



**Agricultural Residues**

**Corn stover**  
**Rice hulls**  
**Sugarcane bagasse**  
**Animal biosolids**



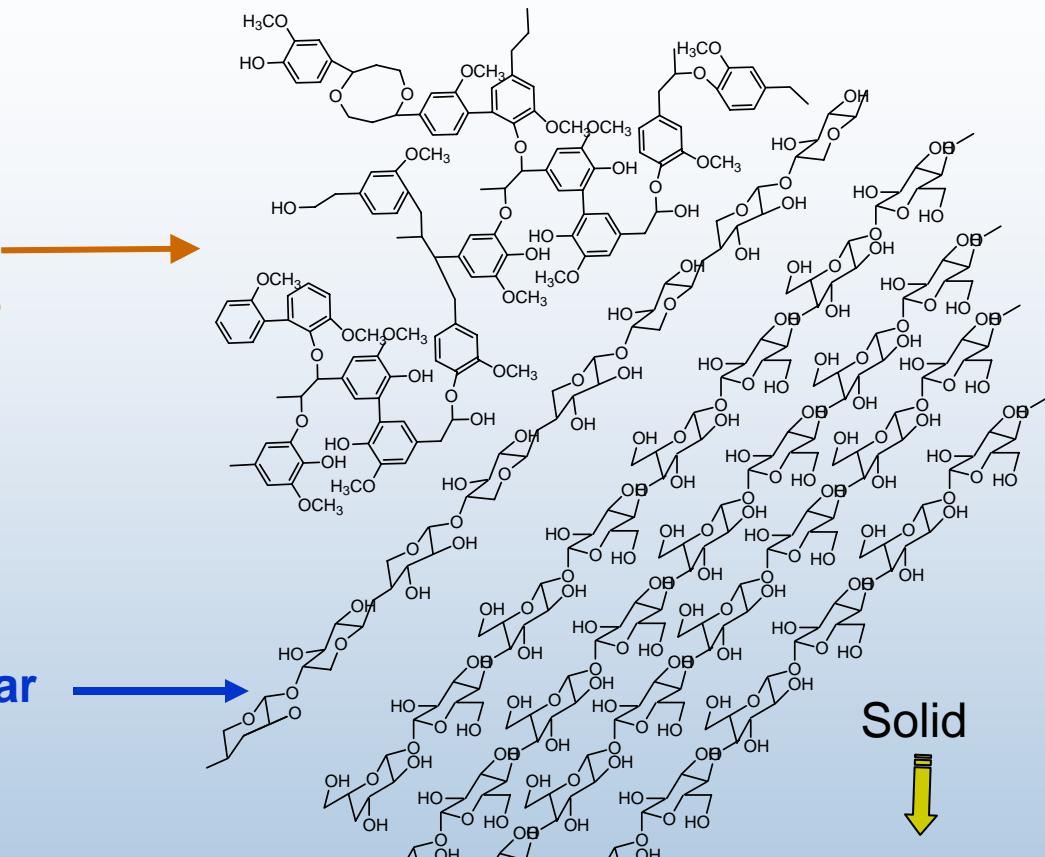
**Energy Crops**

**Hybrid poplar**  
**Switchgrass**  
**Willow**

# Biomass Constituents

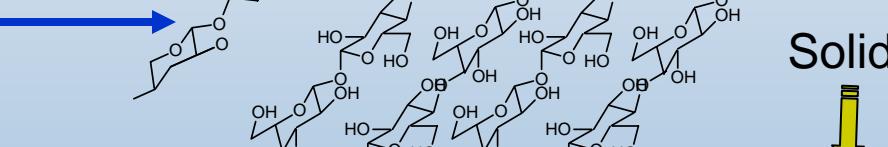
**Lignin: 15-25%**

- ★ Complex aromatic structure
- ★ Very high energy content



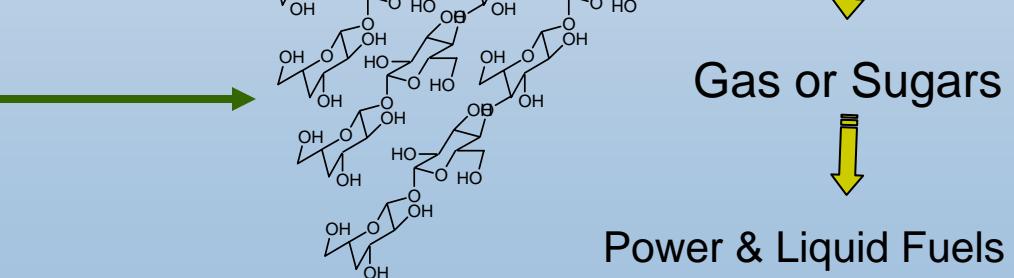
**Hemicellulose: 23-32%**

- ★ Polymer of 5 & 6 carbon sugar



**Cellulose: 38-50%**

- ★ Polymer of glucose, very good biochemical feedstock

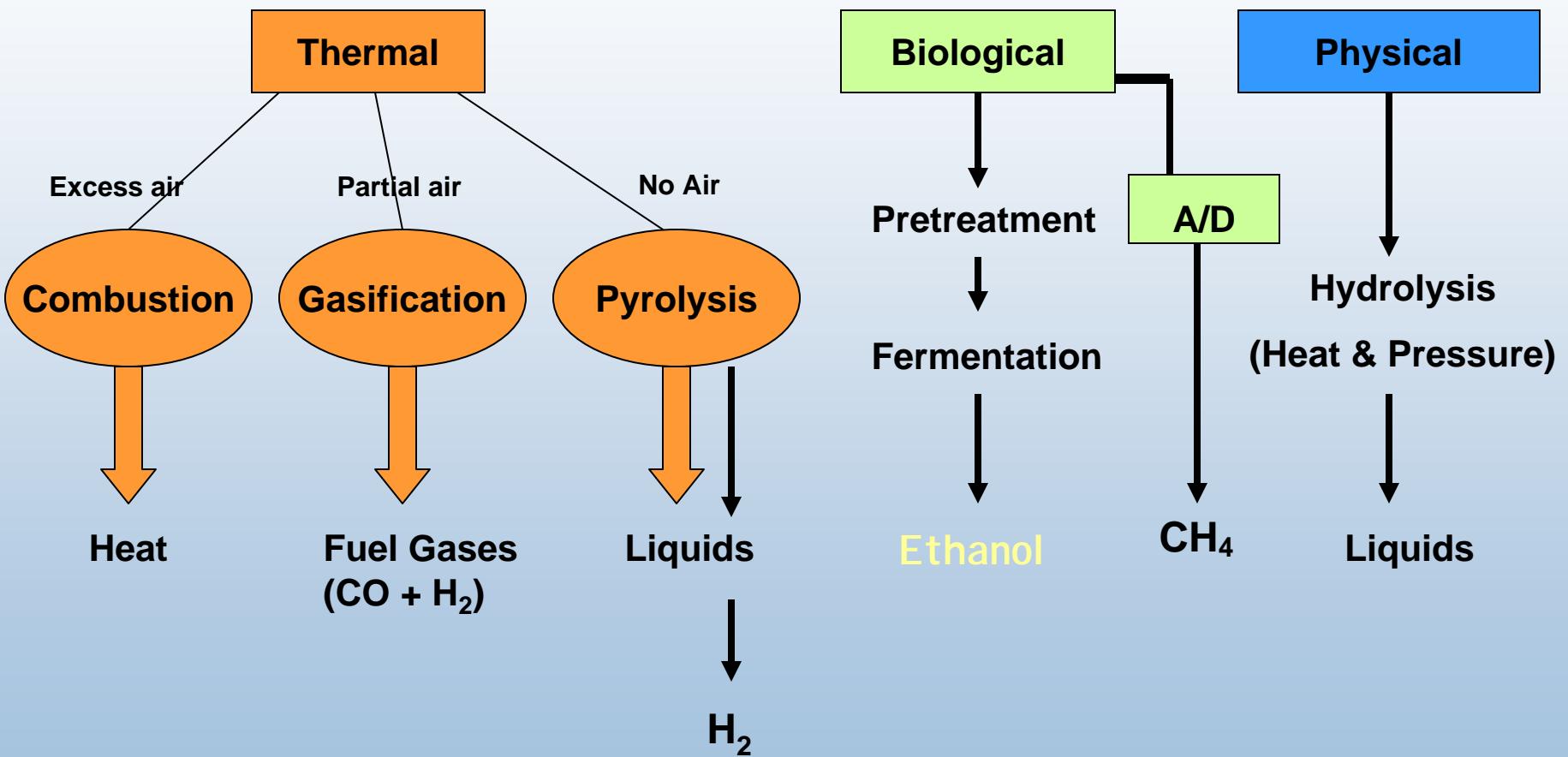


Solid  
↓

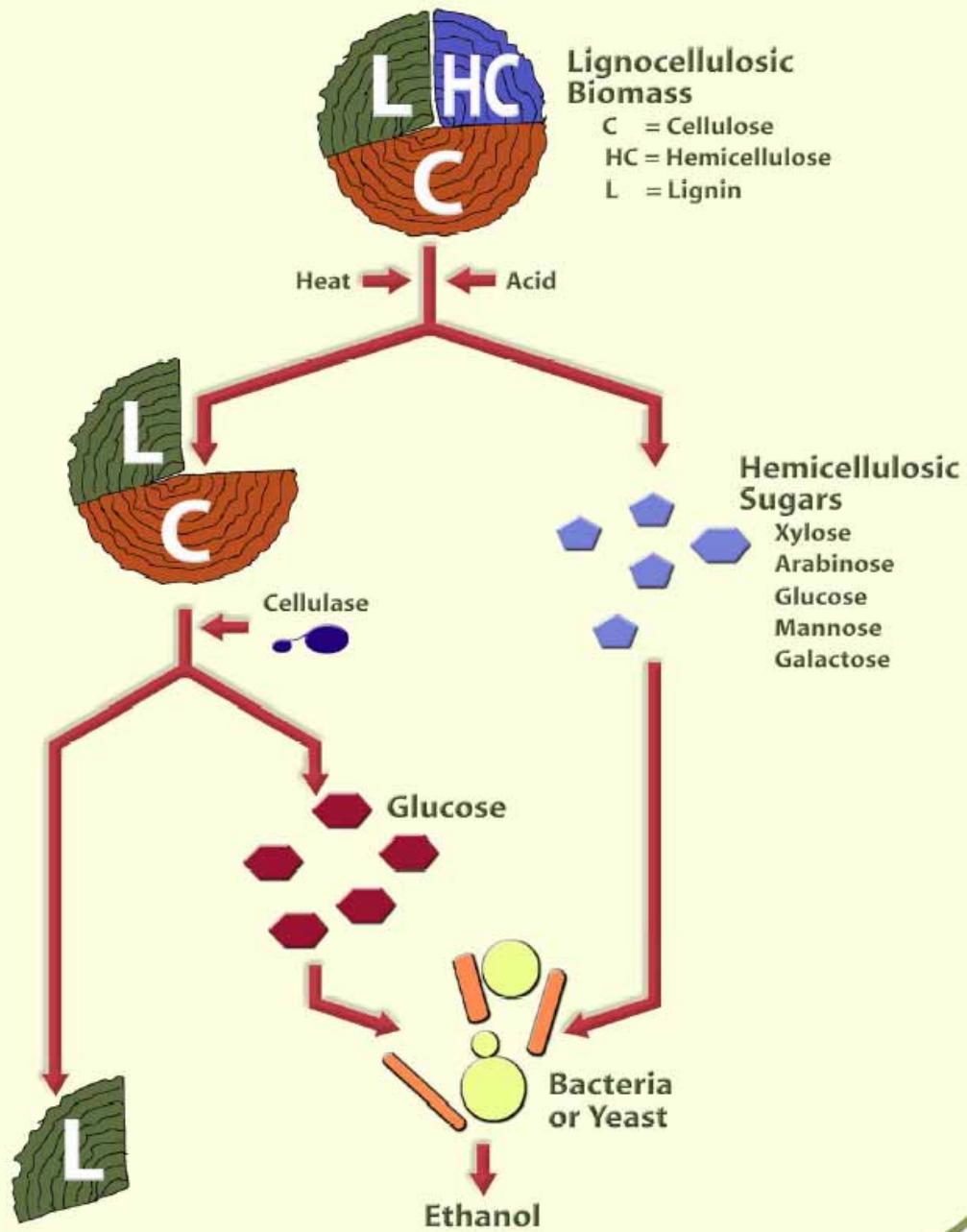
Gas or Sugars  
↓

Power & Liquid Fuels

# Biomass Conversion Pathways



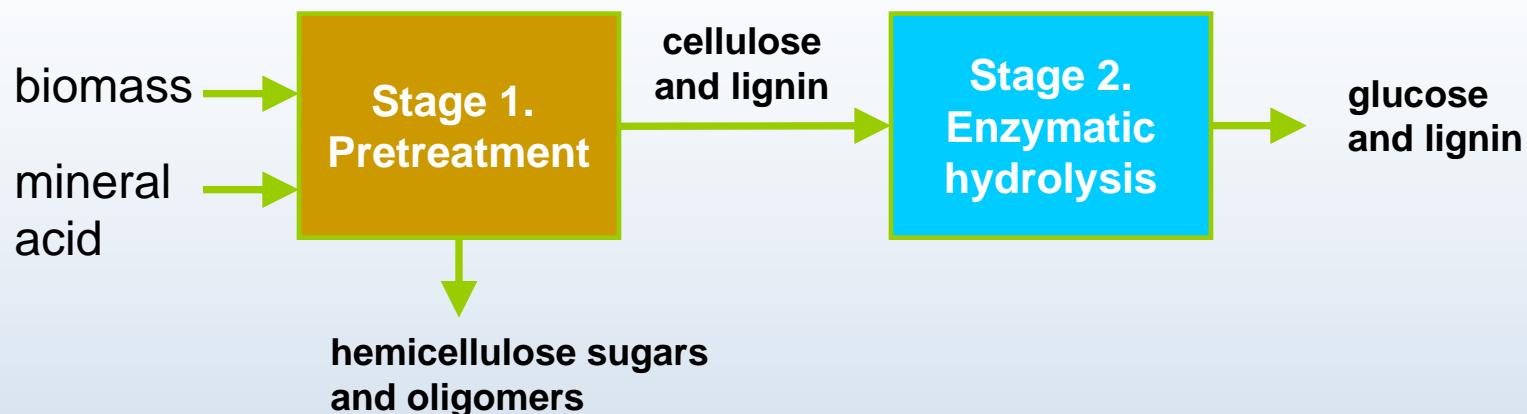
# Fermentation / Pretreatment



Bio-Chemical  
Technology  
Process

*effective for  
converting  
cellulose- and  
hemicellulose-  
into simple sugars*

# The Biomass Saccharification Process

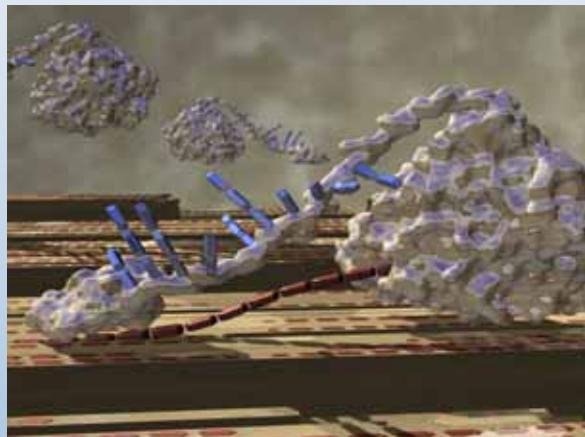


- Mineral acid gives good hemicellulose sugar yields and high cellulose digestibility
- Sulfuric acid usual choice because of low cost
- Requires downstream neutralization and conditioning
- Typical conditions: 100-200°C, 50 to 95% moisture, 0-1%  $\text{H}_2\text{SO}_4$
- Some degradation of liberated hemicellulose sugars
- Current commercial cellulase enzyme preparations release glucose, cellobiose, and some xylose.

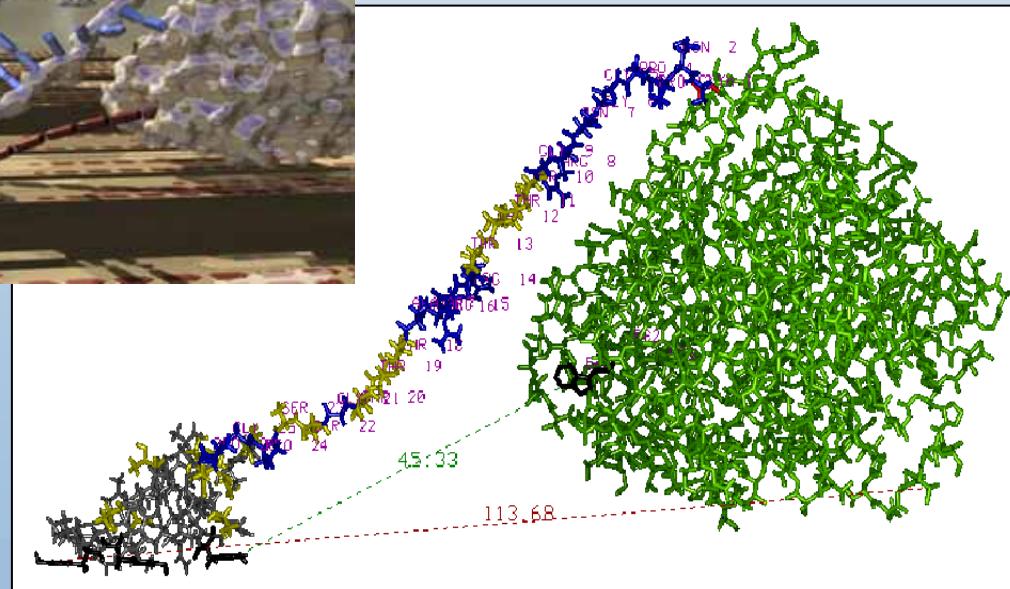
# NREL's Enzymatic Hydrolysis Partnerships

## 3-year Partnerships with Genencor & Novozymes

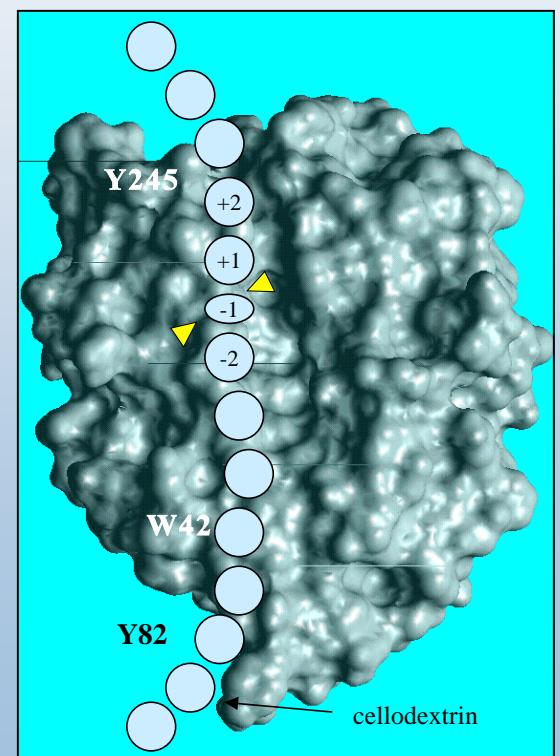
- Enzyme biochemistry and specific activity
- Cellulase - cellulose surface interaction
- Reduce cost of enzyme production (\$0.25/gal)
- Reduce risk to investors



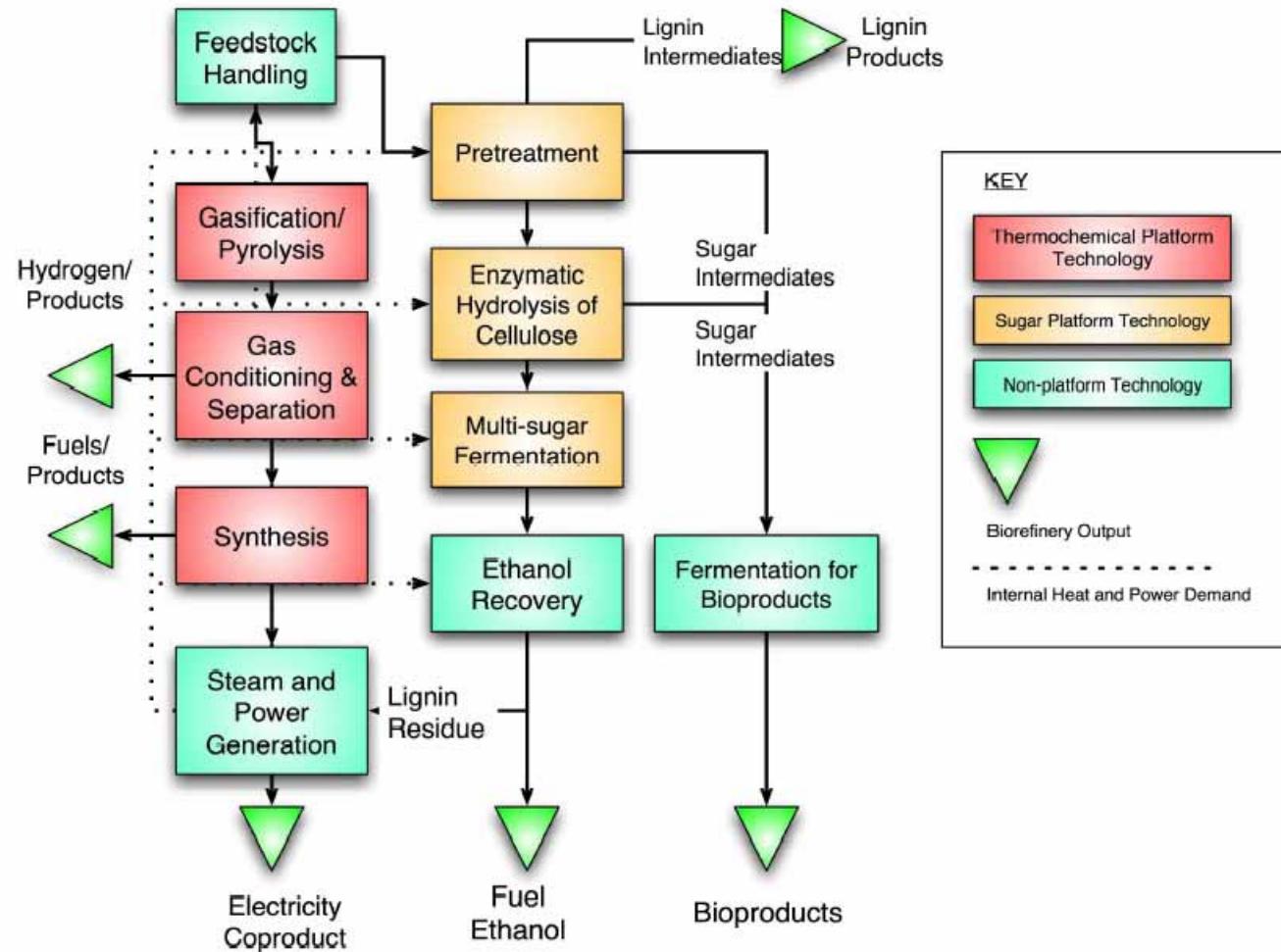
CBH1 from *T. reesei*



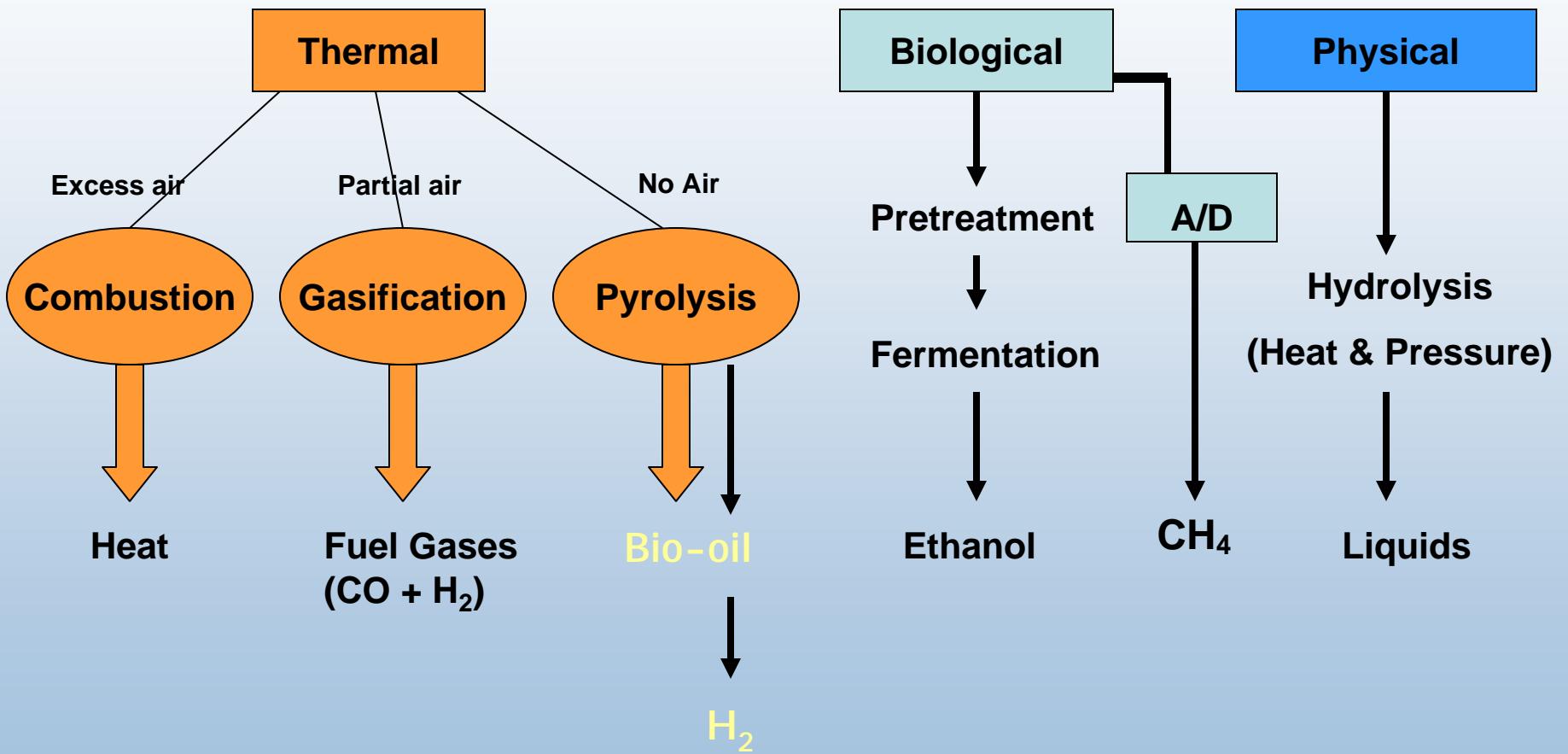
E1 from *A. cellulotiticus*



# Schematic of an Integrated Biorefinery

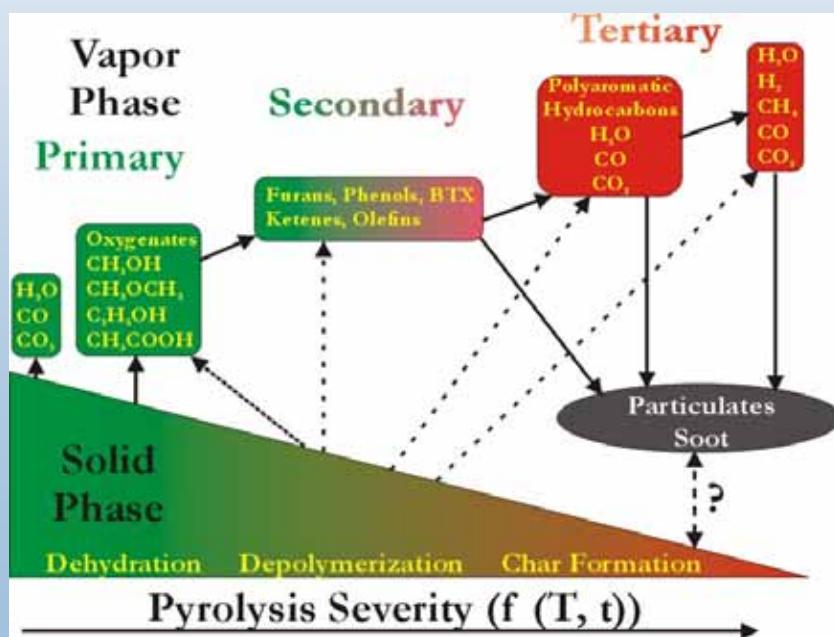


# Biomass Conversion Pathways

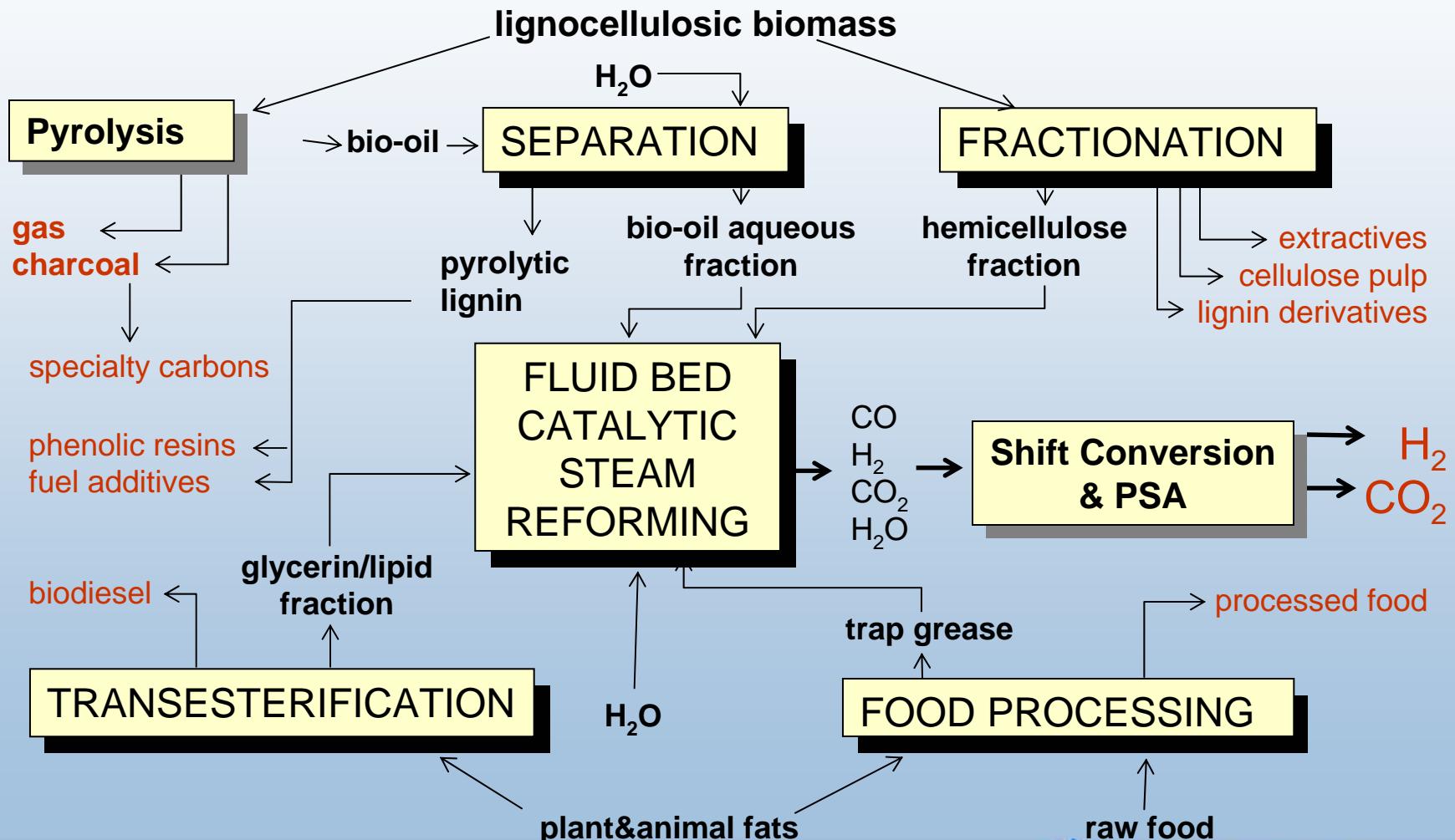


# Pyrolysis Technical Requirements

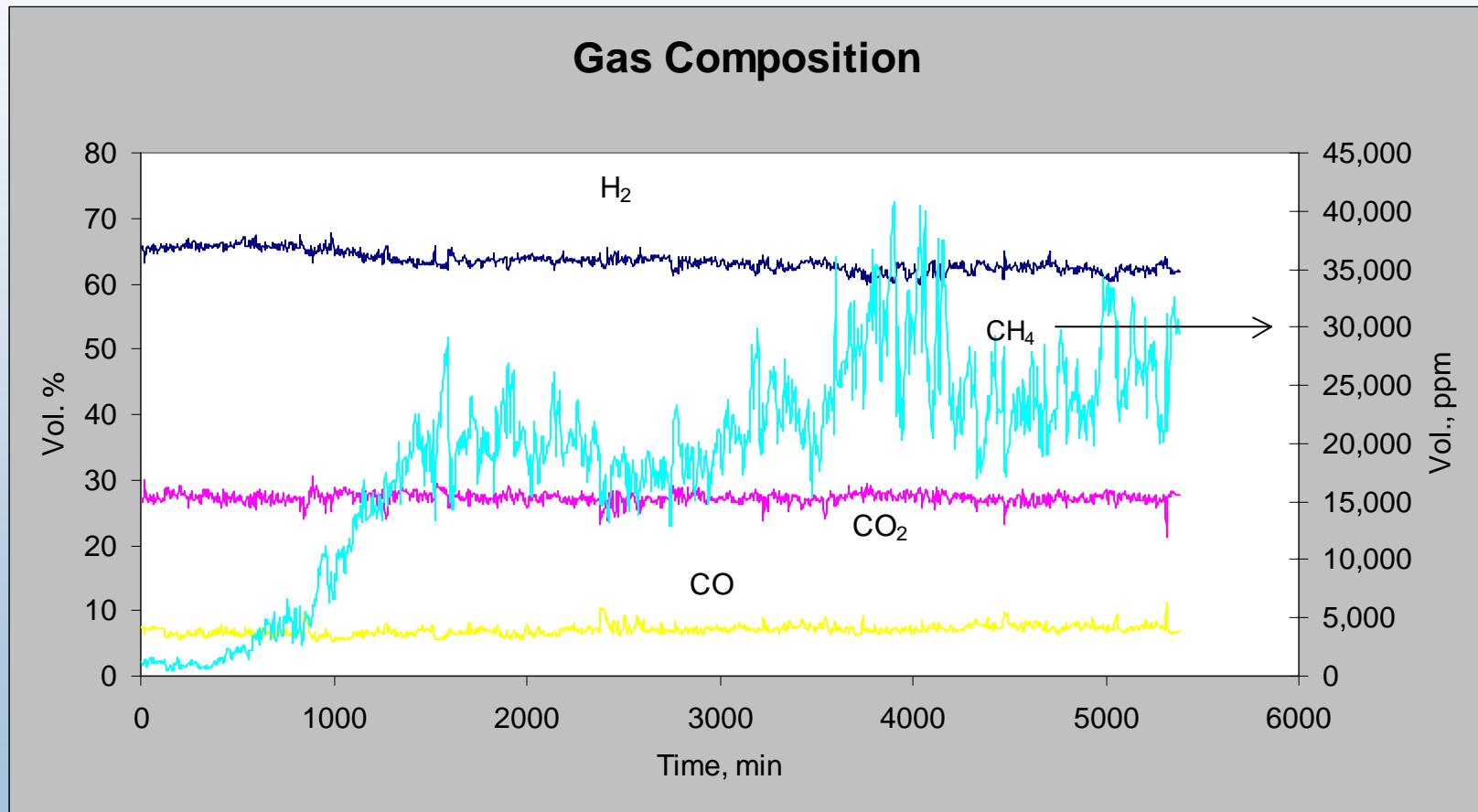
- Rapid heat transfer in the absence of oxygen
- Short residence time at temperature (msec)
- Thermal cleavage of macropolymer bonds (lignin, cellulose, hemicellulose)
- Liquids (70%), gas (15%), Char (15%)



# Bio-oil Refinery Approach



# Bio-Oil Aqueous Fraction Fluidized Bed Reforming



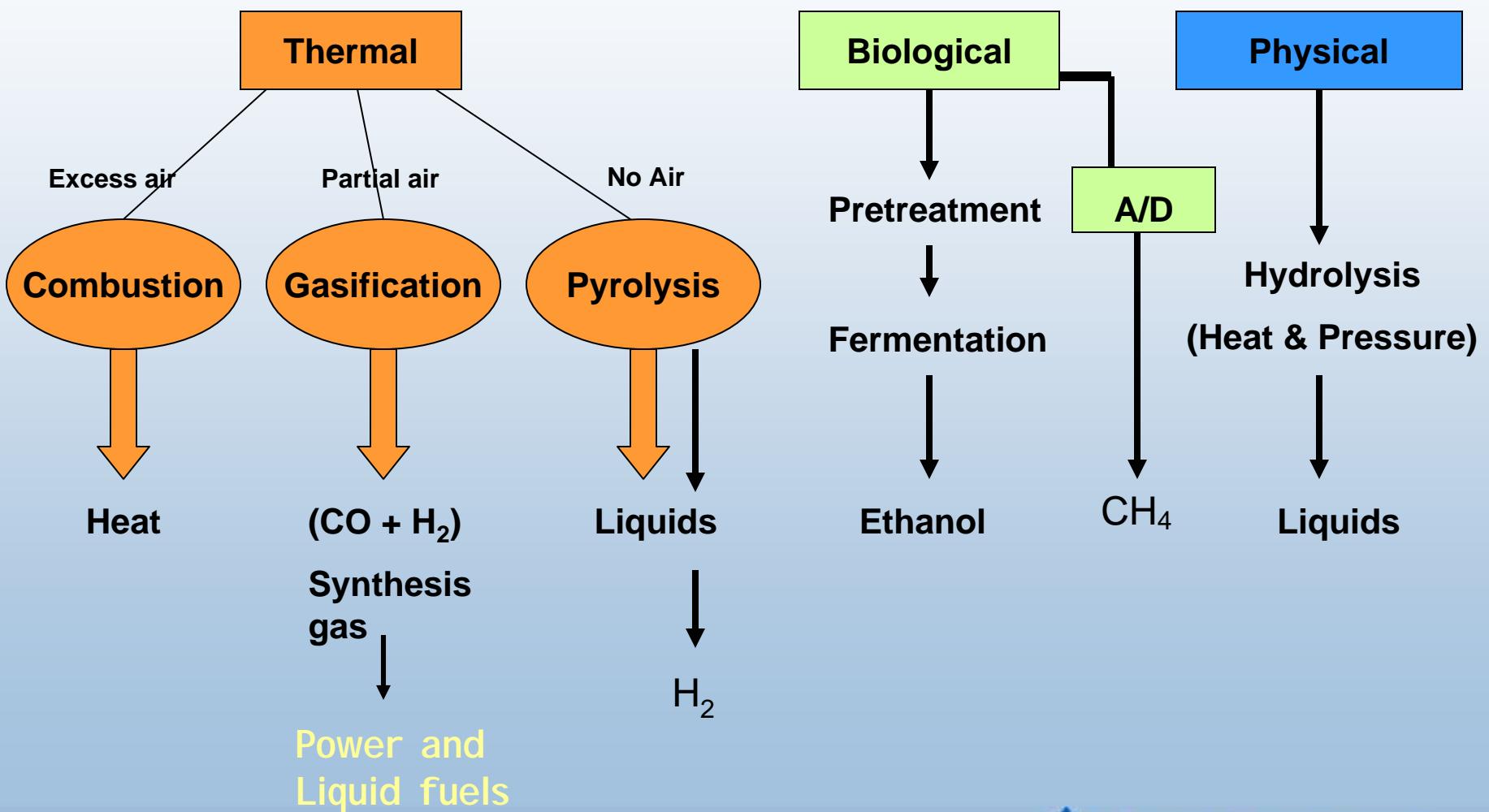
# Bio-Oil From Pyrolysis

## Potential Markets / Products

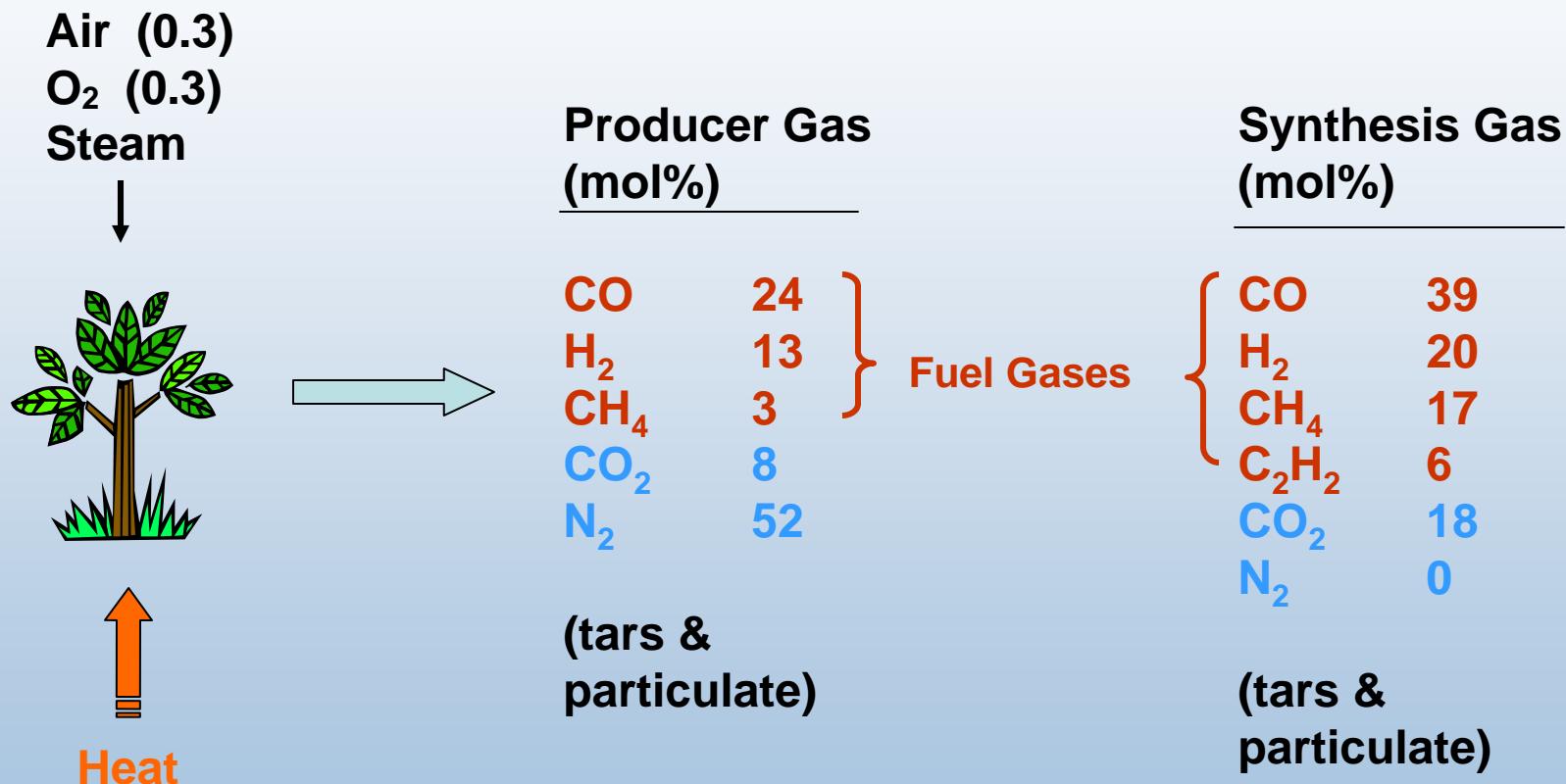
- Liquid boiler fuel substitute
- Reform to Hydrogen
- Food flavorings / Specialty chemicals
- Phenolic replacements
- Asphalt binders



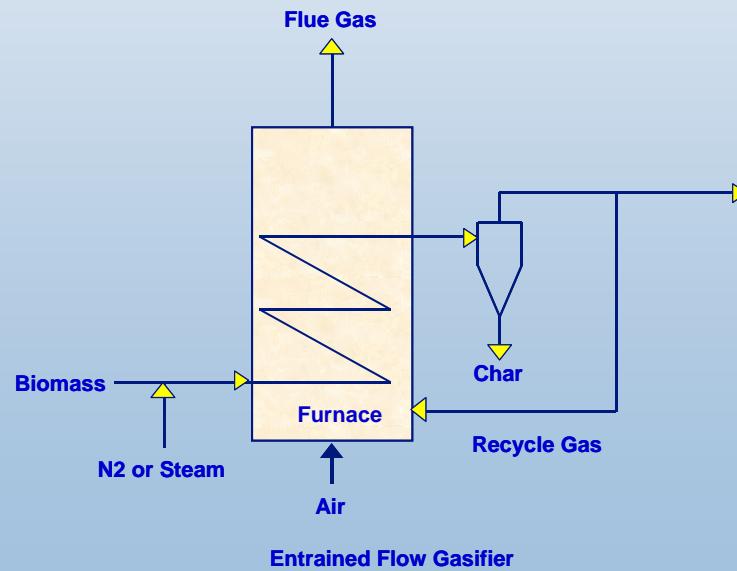
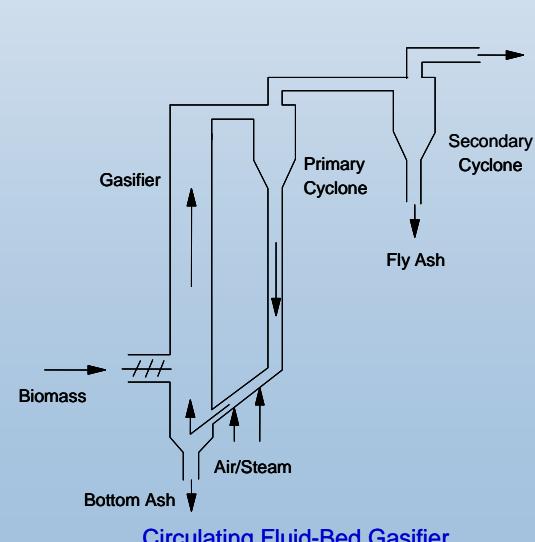
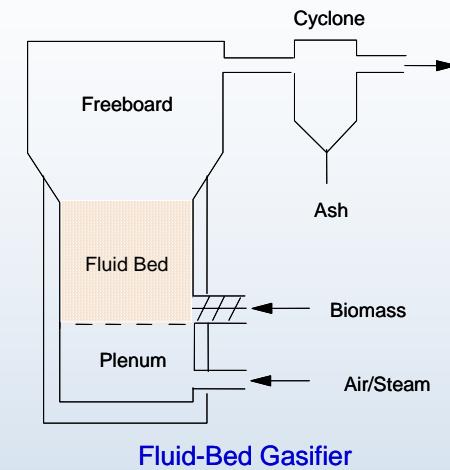
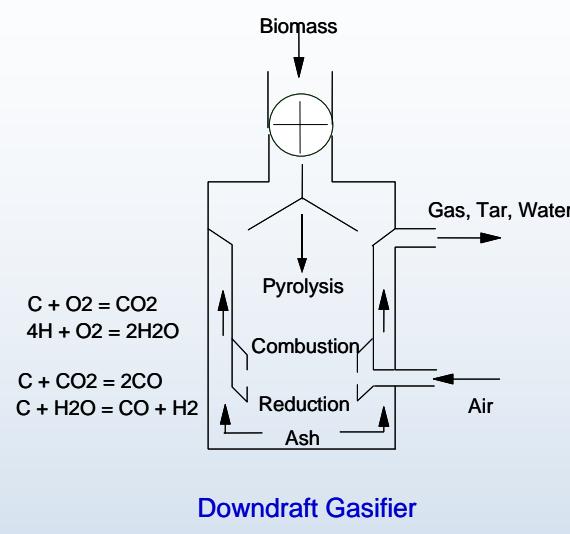
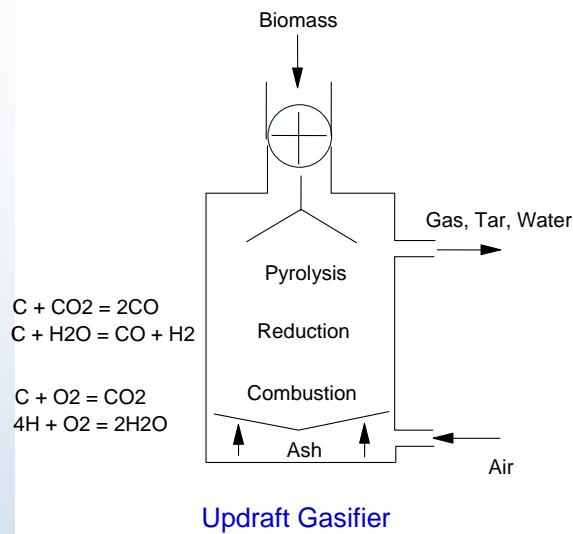
# Biomass Conversion Pathways



# Gasification



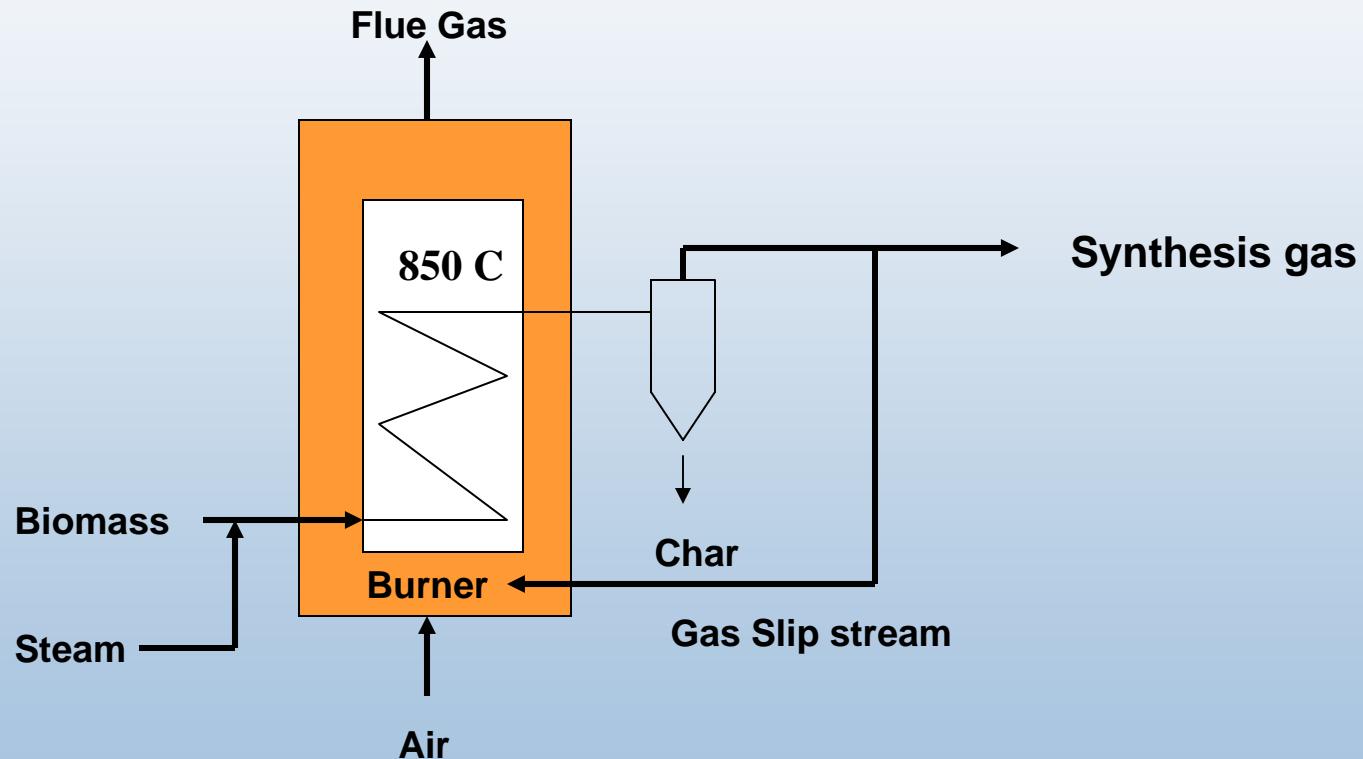
# Different Gasifier Designs



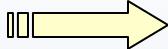
# Entrained Flow Gasification

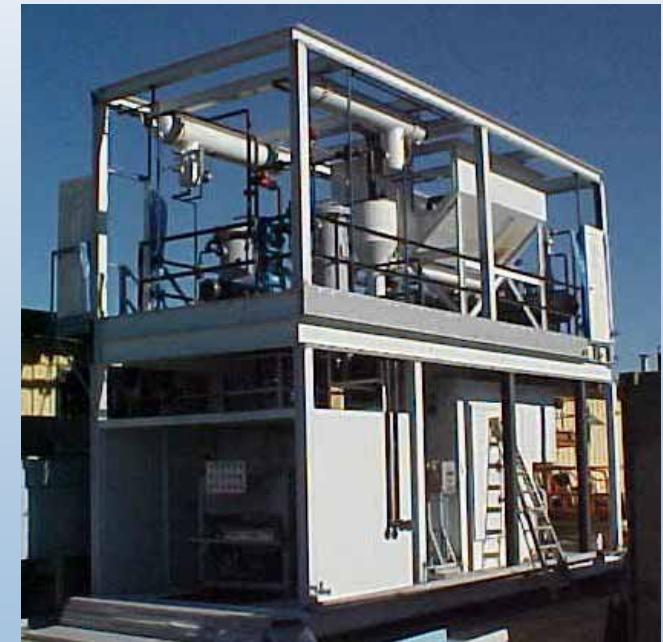
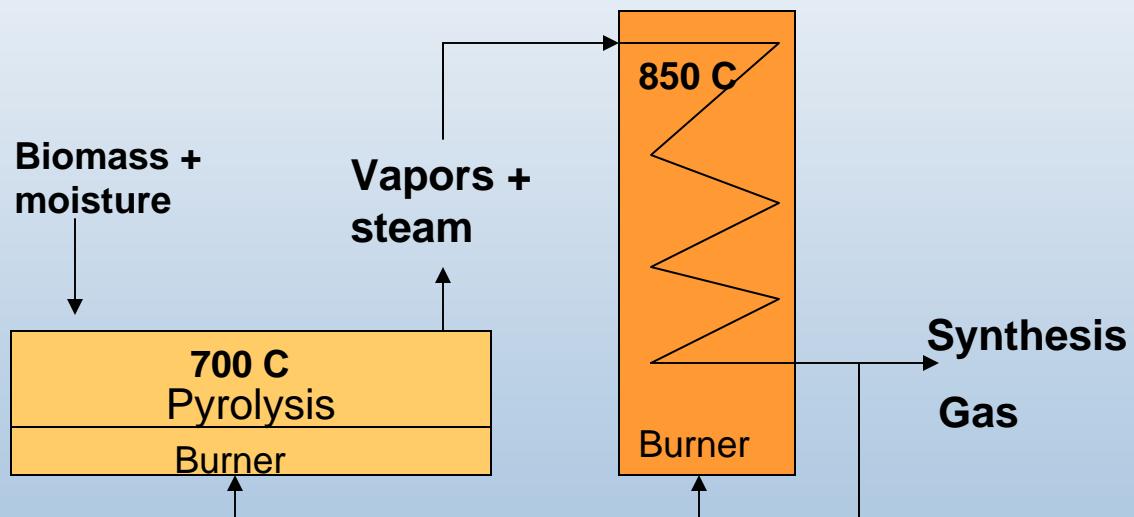
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## (Steam Reforming)



# Staged Gasification

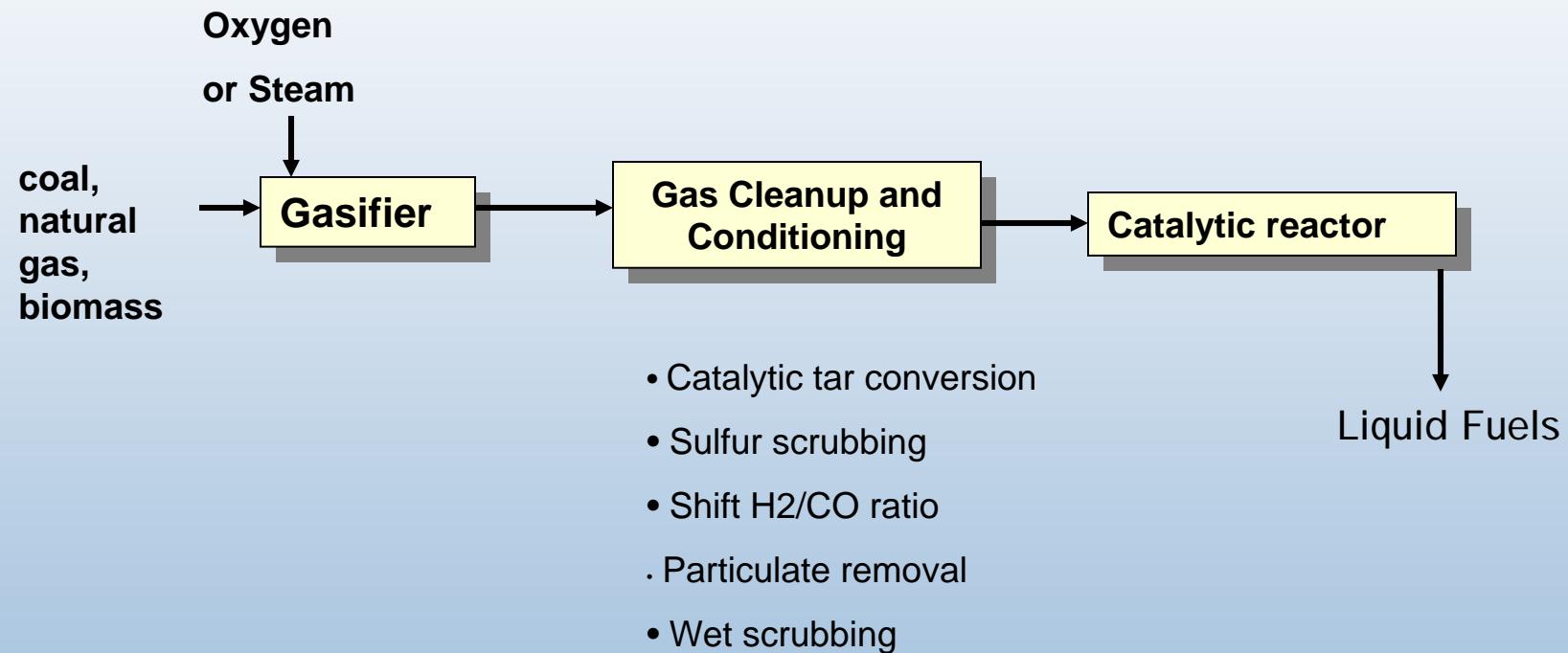
Pyrolysis  Steam Reforming



Carbon Conversion Technologies 2004

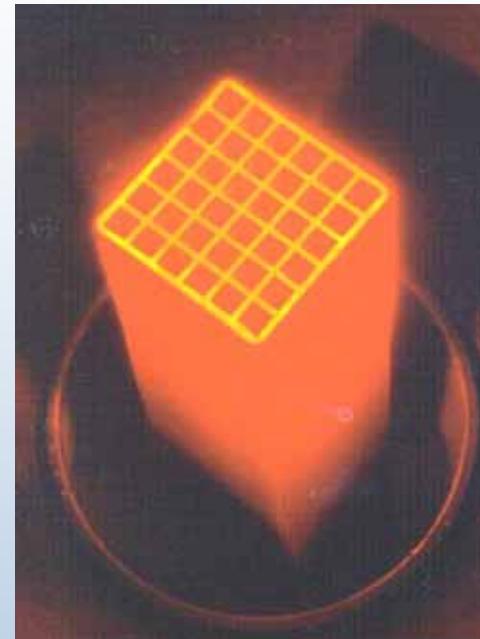
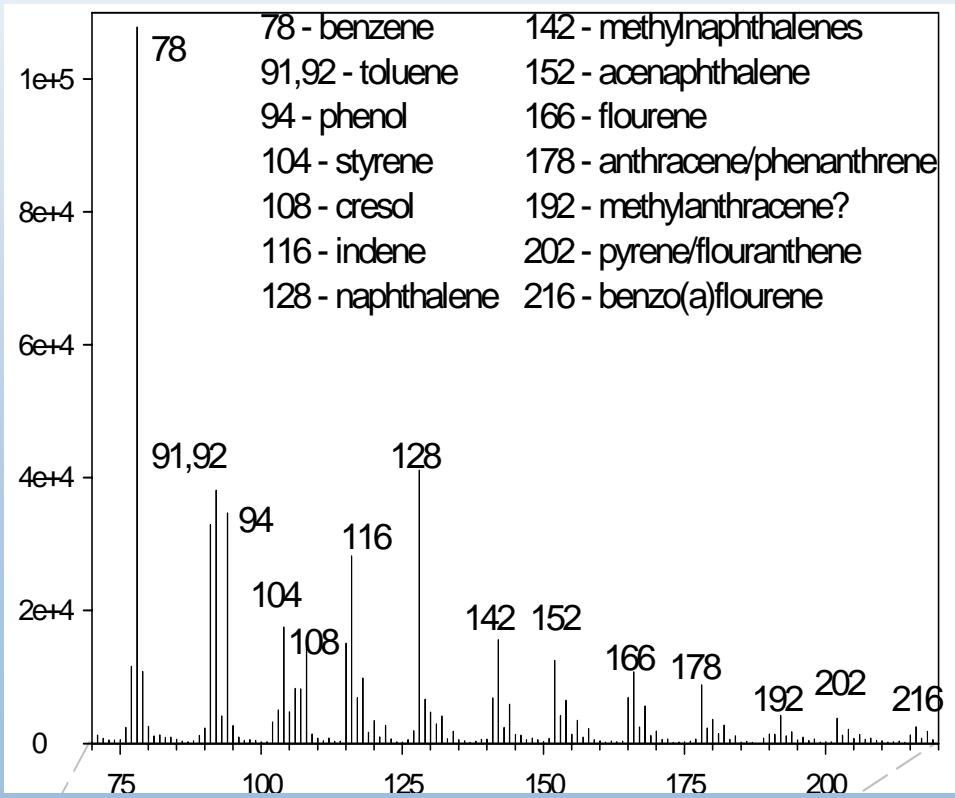
# General Process Description

## Syngas-to-Liquids



# NREL TCPDU Product Gas Tar Composition

Averaged mass spectrum (TMBMS) of tars from indirect wood gasification



Source: VTT Research Center, Finland

Tars can be reformed to additional H<sub>2</sub> + CO

- Nickel catalysts
- 850 ° - 900° C

# Syngas Conditioning

## Gasification Reactions



800° - 850° C



Control of temperature and steam content adjusts H<sub>2</sub> / CO ratio in Syngas

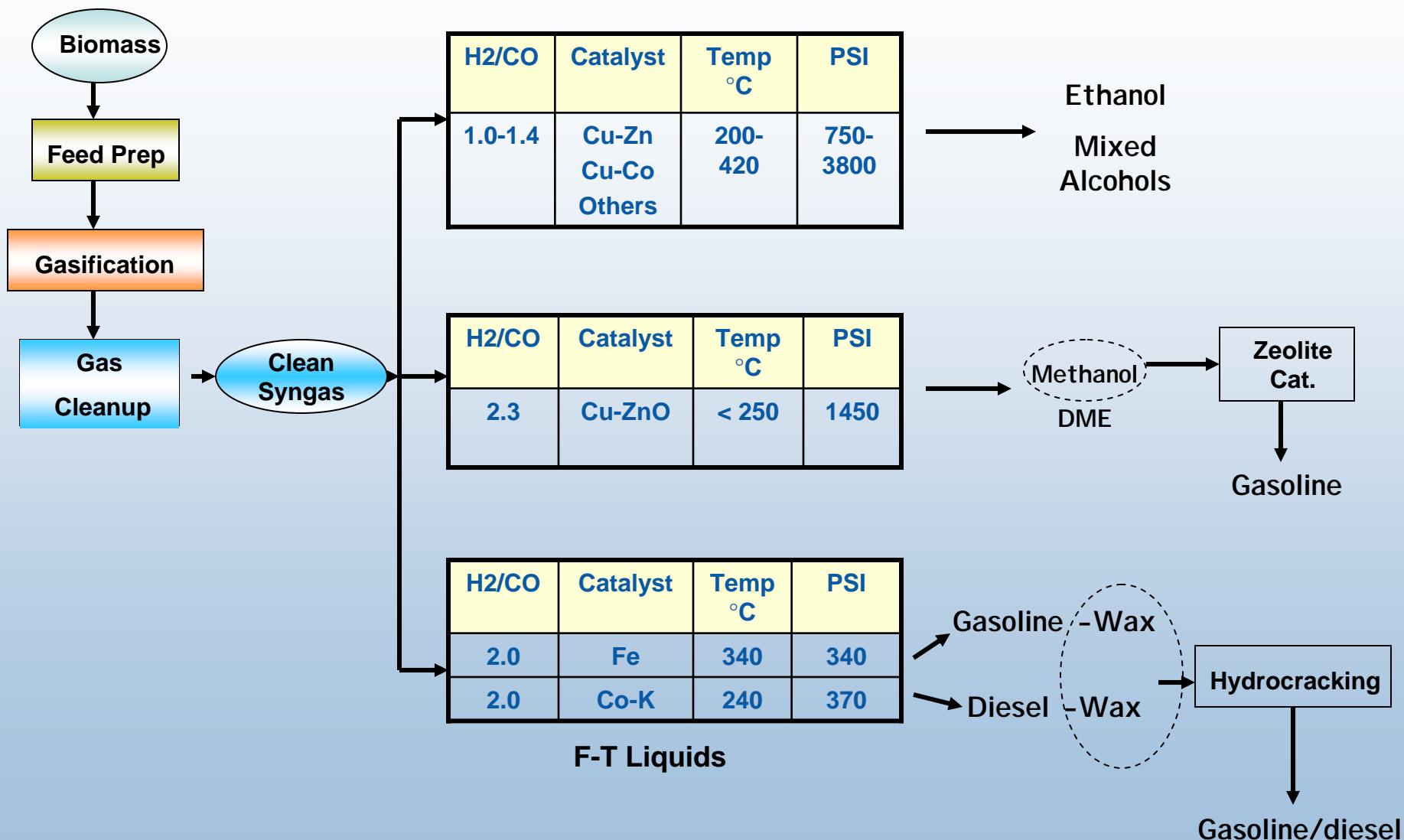
# Gas Cleanup Requirements

## For Fischer-Tropsch gas-to-liquids

Impurity	Removal level
H <sub>2</sub> S, NH <sub>3</sub> , HCN	< 1 ppmv
HCl	< 10 ppbv
Soot, dust, ash	Essentially completely
Tars	Below dew point < 1 ppmv

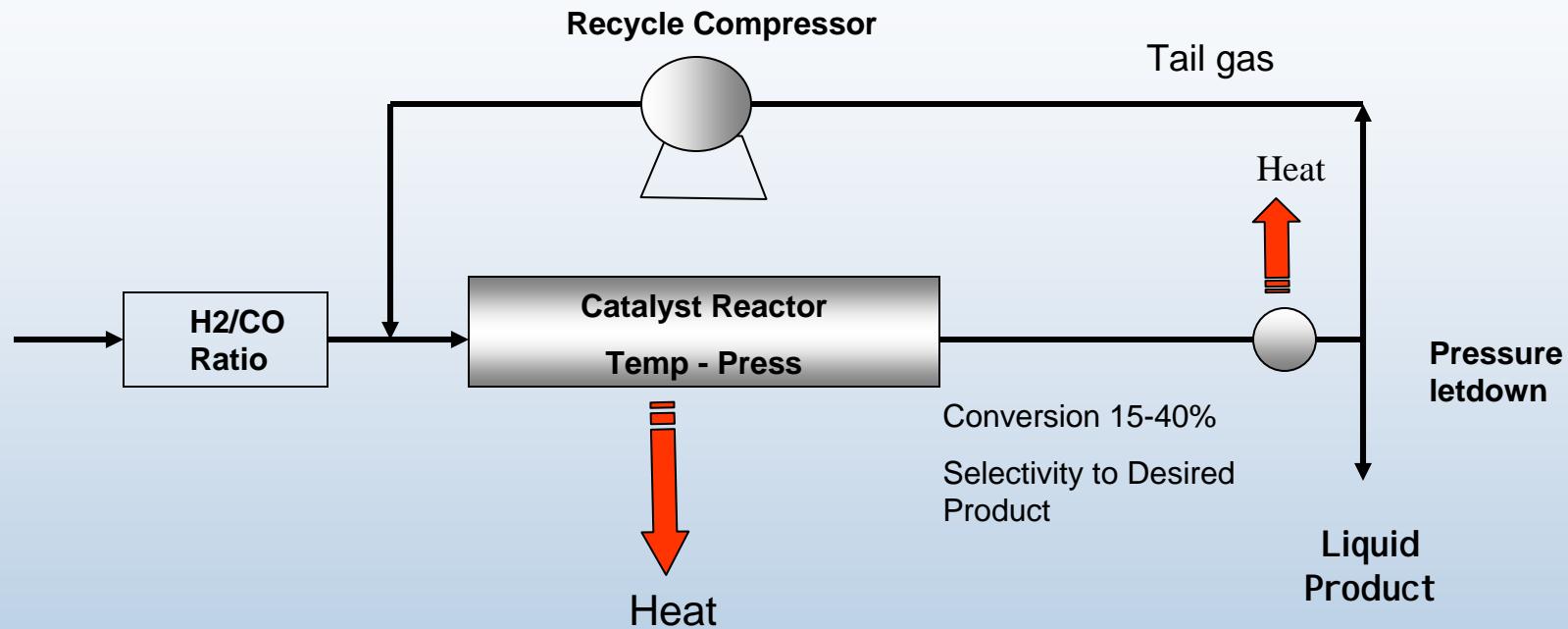
Source: H. Boerrigter et al, October 2002

# Syngas to Liquid Fuel Options



Source: NREL/TP 510-34929

# Gas to Liquids Process Issues



- Syngas Conditioning (cleanup)
- Gas recycle costs
- Heat removal (highly exothermic)

# Liquid Fuel Properties

## F-T Diesel (high quality)

Cetane	> 70 (conventional 45-50)
Total aromatics	< 3 (vol. %)
Polycyclic aromatics	< 0.01 (mass %)
Sulfur	< 1 (ppm)

Source: [www.sasol.com](http://www.sasol.com)

## Mixed Alcohols

Type	Wt%
Methanol	5-30
Ethanol	45-75
Propanol	15
Butanol	5
Pentanol	3
Hexanol & higher	2

Source: Taylor (2002)

# Commercial History of Gas-to-Liquids

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- SASOL (South Africa) 1955
  - Coal → CH<sub>4</sub> → hydrocarbon fuels/chemicals
- Shell (Malaysia) 1993, 12,000 bbl/day
  - Natural gas → syngas → gasoline
- BP / Davy Process Tech (Alaska) 2002
  - Stranded CH<sub>4</sub> → short chain hydrocarbons
  - Compact, modular design
  - Small barge mounted plants under development
- Syntroleum (Australia) under construction/shakedown

# Economic Comparisons

## Biomass to F-T Liquids vs. Electricity

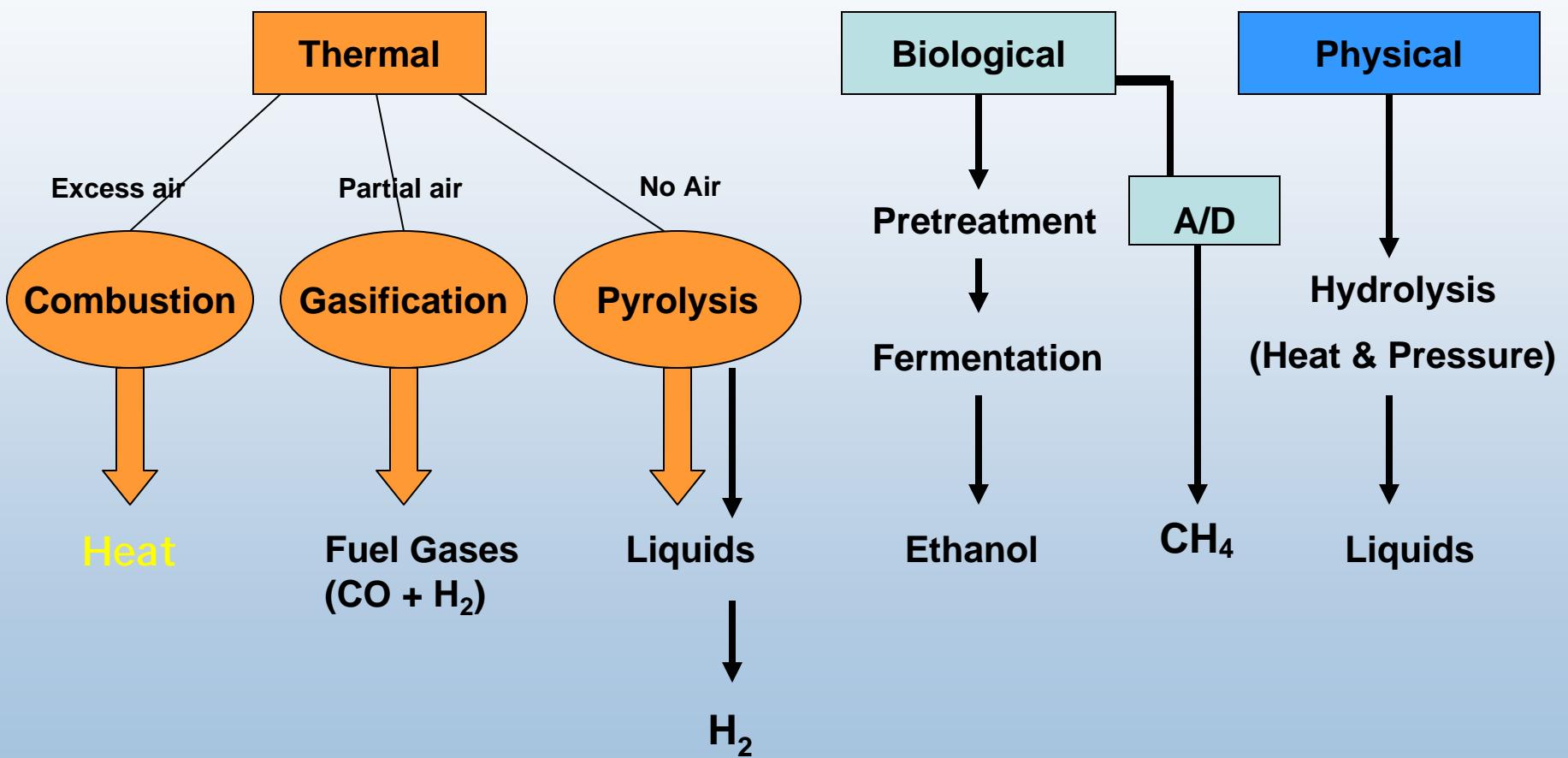
Yield	Value	\$/ton biomass
(1) 79.8 gal/ton	\$1.14+.21=\$1.35/gal (3)(4)	\$108
(2) 455 kWh/ton (combustion-steam turbine)	Purchase agreement \$0.02-.04 / kWh	\$9 - \$18
	Levelized COE \$0.07 / kWh (2)	\$32

Basis:

50 wt% conversion biomass to syngas

1. 10,000 ft<sup>3</sup> syngas/bbl syncrude (Hydrocarbon Processing Feb 2003)
2. 455 kWh/g ton biomass, \$.07/kWh COE (McNeil Technologies Nov 2003)
3. EIA current diesel production cost (May 9, 2004)
4. EIA estimate of FT diesel premium value - \$9/bbl

# Biomass Conversion Pathways



# Biomass Combustion for Heat

- Increasing interest
  - Industrial parks
  - Multiple buildings (district heating)
- High natural gas costs



Source: BioEnergy Corp.  
Nederland, CO

# Biomass Power Applications

- **Combustion / steam turbine – mature but low efficiency**
- **Small modular systems - emerging technology**
- **Gasification combined cycle – under development**



**Biomass is the only renewable resource that causes problems when it is NOT used!**

