
Relationships of McMillan-Mayer and Lewis-Randall Framework

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Introduction

- The need for a thermodynamic framework for prediction and correlation of phase equilibria
 - ◆ Dilute systems containing electrolytes, polymers and biomolecules
- The need for simultaneous models describing various phase equilibria
 - ◆ Hydrate equilibria containing alcohols, salts, etc.
 - ◆ High pressure equilibria containing electrolytes
- Thermodynamic inconsistency between thermodynamic models
 - ◆ MSA, Debye-Hückel, etc. : McMillan-Mayer frameworks
 - ◆ UNIQUAC, NRTL, SAFT etc. : Lewis-Randall frameworks

Comparisons of McMillan-Mayer and Lewis-Randall

- McMillan-Mayer

- ◆ The solvent molecules are replaced by a dielectric continuum.
- ◆ An osmotic experiment where the solvent chemical potentials are kept constant.
- ◆ Neglecting the effect of solvent-solvent and solvent-solute interactions.
- ◆ Independent variables : temperature, pressure

chemical potentials of solvents and numer of moles of solutes

Solvents $I=1, \dots, M$ T, P_0, X'	Solvents $I=1, \dots, M$ Solute $J=M+1, \dots, N$ $T, P=P_0+\Pi, X$
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Comparisons of McMillan-Mayer and Lewis-Randall

- Lewis-Randall(MR) Framework
 - ◆ An analysis under constant temperature and constant pressure
 - ◆ Independent variables : temperature, pressure

number of moles of solutes

Solvents and Solutes

T, P, X

Comparisons of McMillan-Mayer and Lewis-Randall

- Isothermal Gibbs-Dühem equation

- ◆ Lewis-Randall

$$VdP = \sum_{i=\text{solvents}} N_i d \ln \gamma_i + \sum_{j=\text{solutes}} N_j d \ln \gamma_j$$

- ◆ McMillan-Mayer

$$VdP = \sum_{j=\text{solutes}} N_j d \ln \gamma_j$$

- It is impossible to obtain the expression for the chemical potentials of solvents in the McMillan-Mayer frameworks.

Conversion of MM to MR (Haynes et al., 1998)

- Legendre Transformation from Q to Ξ

- ◆ Changes of independent variables from $T, V, \text{ moles numbers}$ to $T, V, \text{ and chemical potentials}$

- ◆
$$\Xi(\mu_0, \mu_1, T, V) = \sum_{N_0} \sum_{N_1} \exp\left(\frac{N_0\mu_0 + N_1\mu_1}{N_{Av}kT}\right) Q(N_0, N_1, T, V) \quad (1)$$

- ◆
$$A = -kT \ln Q \quad \text{and} \quad PV = kT \ln \Xi \quad (2)$$

- ◆ By comparison of equation (1) and (2)

$$-PV = A - n_0\mu_0 - n_1\mu_1 \quad (3)$$

Conversion of MM to MR (Haynes et al., 1998)

- Transformations of mole numbers to chemical potentials of solvent as independent variables by Legendre transformation

- $$A'(T, V, \mu_0, n_j (j \neq \text{solvent})) = A(T, V, n_i (i = \text{all species})) - n_0 \mu_0$$
(4)

- In equation (4), A' is the natural thermodynamic potential working in the McMillan-Mayer framework.

- Excess Pressure

- ◆ Solvent contribution such as hydration or ordering effects

- ◆
$$RT \ln \gamma_i(LR) = \mu'_{i,EX}(MM) - \bar{V}_i P_{EX}(Long - range)$$

Conversion of Experimental Data (Lee, 2000)

- Osmotic coefficients

$$\ln a_w = -\phi^{LR} \frac{\sum_i m_i}{1000/M_w} = -\frac{P_{osm} \langle \bar{V}_w \rangle}{kT} = -\phi^{MM} \rho \langle \bar{V}_w \rangle$$

- Activity coefficients

$$RT \ln \gamma_i^{MM} - RT \ln \gamma_i^{LR} = \beta P_{osm} \langle \bar{V}_i \rangle = \phi^{MM} \rho \langle \bar{V}_i \rangle$$

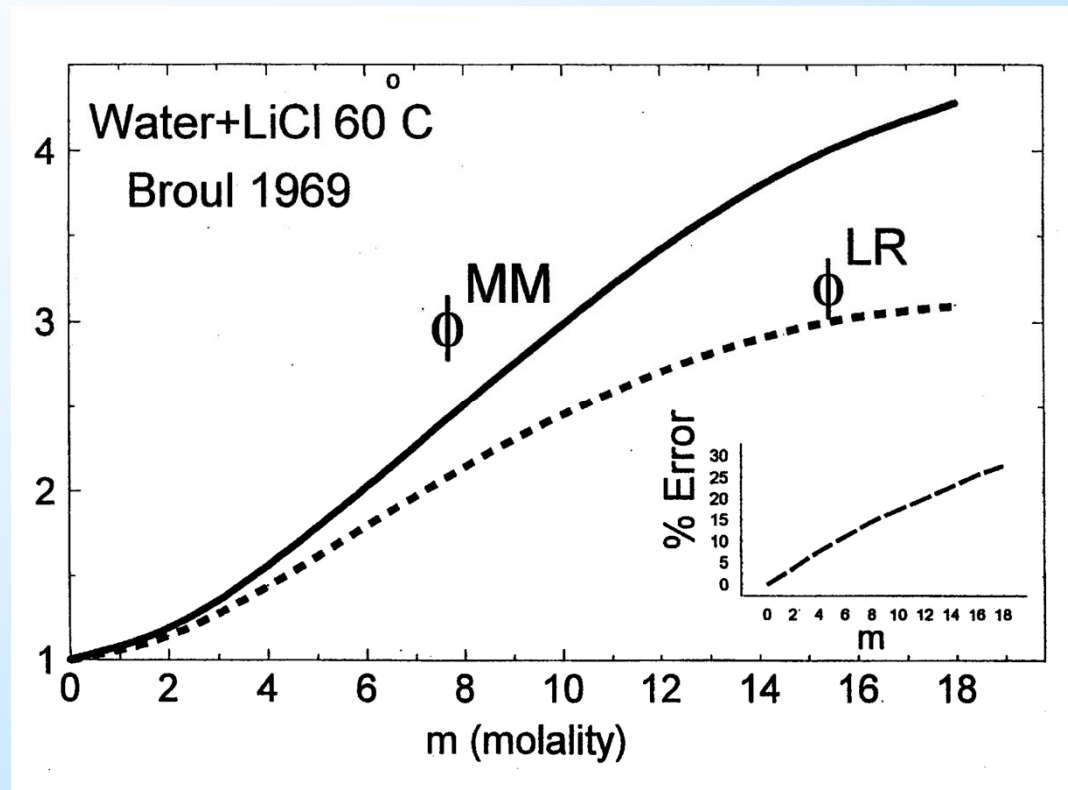


Figure 1. Osmotic coefficients MM and LR for water+LiCl system at 60°C

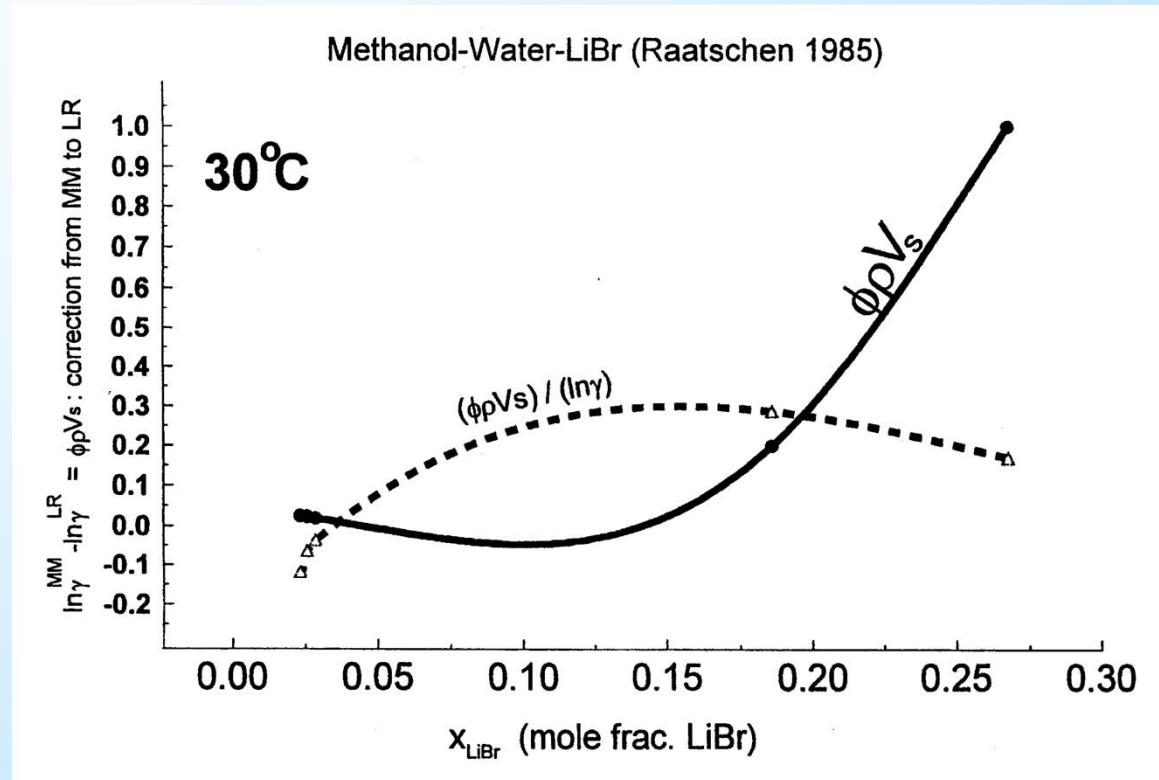


Figure 2. Correction (solid line) and ratio to total $\ln \gamma^{\text{LR}}$ (dashes)

Conclusion

- The comparison of MM and LR framework was accomplished
- The conversion of MM to LR framework was carried on by Legendre transformation.
- The deviations between MM and LR framework were investigated using the experimental data.

References

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