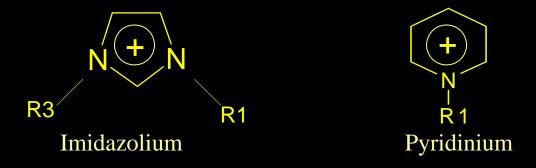
# Solubilities of Gases in the Ionic Liquids

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#### Introduction

## What is the Ionic Liquids?

- Organic salts composed of cations and anions around room temperature
- First Ionic Liquid reacted with water to form highly corrosive compounds
  - N-ethylpyridinium bromide-aluminium chloride melt (Hurley et al., 1951)
- Two main groups of ionic liquid
  - Water and air stable



# Structure of Ionic Liquids

#### **Cations**

- Based on Imidazolium, Pyridinium (organic compounds)



#### Anions

- Inorganic compounds

$$[BF_4]^ [CF_3CO_2]^ [PF_6]^ [NO_3]^ [EtSO_4]^-$$

Schematic of the structure of [bmim][PF<sub>6</sub>]

# Preparation of Ionic Liquids

- Imidazolium based Ionic Liquids
  - Reaction of N-alkylimidazole, RIm,
    with alkyl salts (R'X) in appropriate organic solvents
  - (1)  $X^-$  is the anion of interest  $RIm + R'X \longrightarrow RR'Im^+X^-$
  - (2) Fist step, alkylimidazolium halides are synthesized  $RIm + R'X' \longrightarrow RR'Im^+X'^-$  X'=Cl, Br, Il
  - (3) Anion exchange corresponding acids of their salts  $RR'Im^+X'^- + MX \longrightarrow RR'Im^+X^- + MX'$

§ The choice of cation M is important §

# Properties

# Physical Properties

- Melting point (-96°C ~)
  - Melting point is lowered as increasing length of alkyl chain in cations
  - The increasing disruption of crystal packing overrides increased van der Waals interactions between the larger components.

#### Density

- $1.1 \sim 1.6 \text{ g/cm}^3$  at ambient temperature (291~303K)
- The compounds of bulky, and therefore, weakly coordinating anions such as  $CF_3(CF_2)_3SO_3^-$  and  $(CF_3SO_2)_3C^-$  possess relatively high densities regardless of counter ions.

# Properties

- Viscosity
  - Several tens to hundred times that of water at room temperature
  - Longer alkyl chains of cation makes the liquid more viscous.
  - Structure and basicity of anion affects the viscosity.
    - The decrease of the size of anion decreases the van der Waals interaction but increases the electrostatic interaction through hydrogen bonding.

# Application

- Non-volatile, negligible vapor pressure
  - Green chemical solvents
    - Increasing limitations on volatile organic emissions
    - ILs are possible to replace the solvents
  - Distillation with poorly volatile or thermally labile products
  - Extraction using supercritical CO<sub>2</sub>
    - Don't have a cross-contamination
    - Supercritical CO<sub>2</sub> extraction achieved greater than 98% solute recovery for several of the organics

#### (Blanchard et al, I&EC, 2001; Nature, 1999)

- ◆ Measuring the recovery rates of aromatic and aliphatic solutes from [bmim][PF<sub>6</sub>]
- ◆ This work has shown that CO<sub>2</sub> can completely extract a wide array of organic solutes from an ionic liquid.

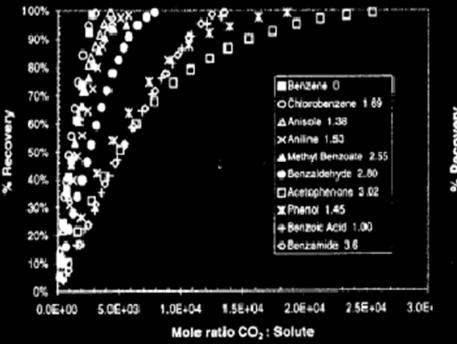


Figure 1. Extraction of aromatic solutes from [bmim][PF<sub>6</sub>] with SCCO<sub>2</sub> at 40 °C and 138 bar

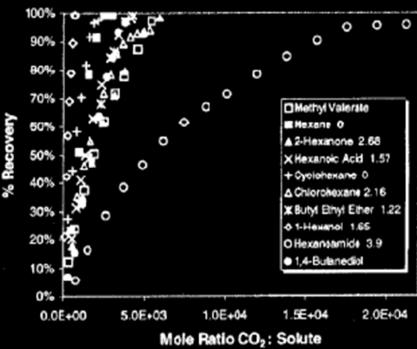


Figure 2. Extraction of aliphatic solutes from [bmim][PF<sub>6</sub>] with SCCO<sub>2</sub> at 40 °C and 138 bar

## Application

- Good solvent
  - High solubility and selectivity with organic, inorganic, organometallic compounds
  - Reaction solvent
  - Used to the liquid-liquid extraction process
- Catalysis
  - Fiedel-Crafts alkylations, Diels-Alder reaction, hydrogenation, hydroformylation etc.

Fig.3. Ionic Liquids permit high yields and selectivity for the Diels-Alder reaction

#### Effects of Ions

- Effect of cations and anions on the ILs properties.
  - Solubilities and Interaction of super critical CO<sub>2</sub> with anions

Table 1. Ionic liquid- $CO_2$  solubility( $X_{CO2}$ ) and liquid molar volumes(mL/mol) at 40, 50 and 60°C and elevated pressures (Blanchard et al., 2001)

	$T = 40^{\circ}C$			$T = 50^{\circ}C$				T=60°C		
Ionic Liquid	P(bar)	$X_{CO2}$	mL/ mol	P(bar)	$X_{CO2}$	mL/ mol	P	(bar)	$X_{CO2}$	mL/ mol
[bmin][PF <sub>6</sub> ]	95.67	0.729	71.2	92.46	0.675	83.9	9:	3.01	0.667	84.5
[C <sub>8</sub> min][PF <sub>6</sub> ]	92.67	0.755	80.2	92.67	0.705	103.0	9:	2.88	0.726	94.8
[bmin][NO <sub>3</sub> ]	92.00	0.513	99.2	92.62	0.530	95.0	9	3.17	0.522	95.9
[C <sub>8</sub> min][BF <sub>4</sub> ]	92.90	0.708	96.9	92.28	0.671	106.1	9:	3.73	0.651	111.5
[N-bupy][BF <sub>4</sub> ]	91.59	0.579	94.0	92.35	0.581	92.2	9.	5.80	0.549	98.1
[emim][EtSO <sub>4</sub> ]	92.68	0.423	121.0	94.27	0.403	124.6	9.	4.61	0.457	111.1

#### Effects of Ions

#### liquid-Liquid Equilibria (Anthony et al., 2001)

- The mutual solubilites of water and  $[C_8min][PF_6]$  are lower than those for the equivalent IL with a short alkyl chain,  $[bmin][PF_6]$
- Changing the anion from [PF<sub>6</sub>] to [BF<sub>4</sub>] increases the mutual solubilities.

Table 2. LLE Results for water with Ionic liquids at ambient conditions

	IL in aqu	eous phase	Water in IL phase			
Ionic Liquid	wt. %	Mol fraction	wt. %	Mol fraction		
[C <sub>8</sub> min][PF <sub>6</sub> ]	$0.7 \pm 0.1$	3.5×10 <sup>-4</sup>	$1.3 \pm 0.5$	0.20		
[bmin][PF <sub>6</sub> ]	$2.0 \pm 0.3$	$1.29 \times 10^{-3}$	$2.3 \pm 0.2$	0.26		
[C <sub>8</sub> min][BF <sub>4</sub> ]	$1.8 \pm 0.5$	$1.17 \times 10^{-3}$	$10.8 \pm 0.5$	0.63		

#### Effects of Ions

- CO<sub>2</sub> Capture by a Task-Specific Ionic Liquid (Eleanor et al. 2001)
  - Interaction between gases and liquid based on separation process
    - Large-scale CO<sub>2</sub> capture is aqueous amines to form ammonium carbamate => loss of capture agent
    - Change the functional group of ionic liquid

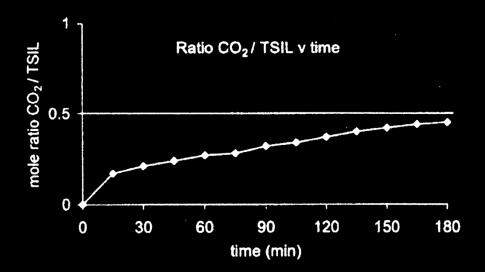


Fig. 4. CO<sub>2</sub>/TSIL molar ratio as a function of time

# Separation of CO2 from gas mixture

- Strong interaction with Ionic Liquid & CO<sub>2</sub>
  - Phase behavior of ILs and pure gases (Jennifer et al. 2002)
    - Ionic liquid : [bmim][PF<sub>6</sub>]
    - Carbon dioxide, ethylene, ethane, methane, argon, oxygen, carbon monoxide, hydrogen, and nitrogen
    - Gases that are less soluble in the IL are less soluble in the other solvents
    - However, carbon dioxide is more soluble in the IL than the other solvents
  - The factor to influence the solubility
    - Large dipole moment has high solubility
    - Chemical interaction anion and CO<sub>2</sub>
    - Due to large quadrapole monent

# Separation of CO<sub>2</sub> from gas mixture

- ILs used by absorber and Supported-liquid Membrane
  - IL can be high selective solvents
    - Used in conventional absorbers
  - Supported-liquid Membrane
    - Limitation conventional liquid slowly evaporate
      - minimum thickness
      - unstable and replenish the solvents

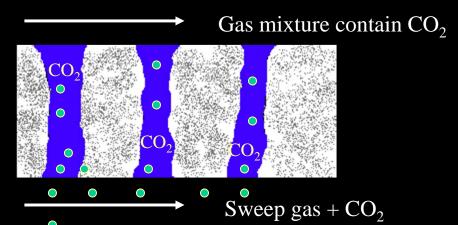


Fig.5. Supported-liquid membrane

# Experimental

- Preparation of ILs
  - 1-hexyl-3-methyl-imidazolium tetrafluoroborate
  - 1-ethyl-3-methyl-imidazolium tetrafluoroborate
    - Investigation of alkyl chain length on cation
  - Certification
    - Assay: more than 99%
    - Water contents: less than 1.0%
  - To leave ILs in the vacuum oven at 55 °C for a week
    - To eliminate water and other gases

# Experimental apparatus

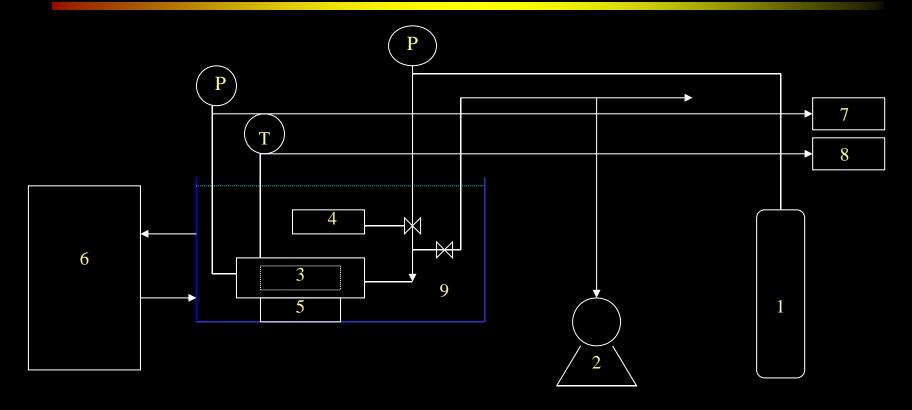


Fig. 6. The experimental apparatus for measurement of the solubility of pure  $CO_2$  gas in the Ionic Liquids

(1) gas bomb; (2) vacuum pump; (3) view cell (4)small cell (5)magnetic stirrer (6) constant T. circulator (7) pressure indicator (8) temperature indicator (9) water bath

# Experimental Method

# Measurement of ILs density at difference temperature

- Using the pycnometer (5  $\pm$  0.005 ml)
- Temperature range : 15 − 30 °C
- To calculate mole ratio and to predict the solubility

# Solubility of Pure CO<sub>2</sub>

- Pressure range : 1 ~ 10 bar
- Measurement of the change of pressure in the view cell containing ionic liquids and pure CO<sub>2</sub>
- Calculate the density of CO<sub>2</sub>
  (Gas property program of University of Idaho )

