



# *Excess Properties*

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# I. Behavior of Excess Properties

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- 1. Excess Gibbs energy, Excess enthalpy, Excess entropy are related by

$$\textcircled{1} \quad g^E = h^E - Ts^E$$

$$\textcircled{2} \quad \frac{g^E}{RT} = \frac{h^E}{RT} - \frac{s^E}{R}$$

$$\textcircled{3} \quad \frac{h^E}{RT} = -T \left( \frac{\partial (g^E / RT)}{\partial T} \right)_{P,X}$$



# Definitions of Regions on the $\hat{g}$ vs. $\hat{h}$ Diagram

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For convenience,

$$\hat{g} \equiv g^E / RT$$

$$\hat{h} \equiv h^E / RT$$

$$\hat{s} \equiv s^E / R$$

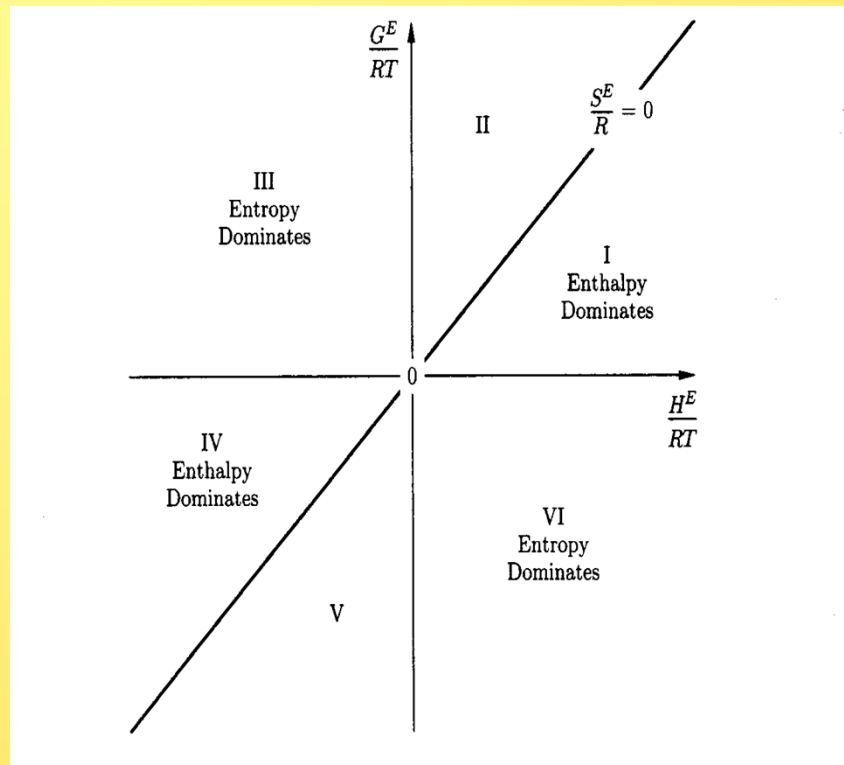
$$\hat{c} \equiv c_p^E / R$$

at  $x_1 = x_2 = 0.5$

- 액체 혼합물의 과잉물성과 상대적 크기들은 공학적 목적이나 관찰된 용액의 거동을 근거로 분자현상을 규명하는데 유용하게 쓰인다.

# Definitions of Regions(I ~ VI)

- Definitions of Regions on the  $\hat{g}$  vs.  $\hat{h}$  Diagram



Region	Sign $G^E$	Sign $H^E$	Sign $S^E$
I	+	+	+
II	+	+	-
III	+	-	-
IV	-	-	-
V	-	-	+
VI	-	+	+

## 50°C 의 6성분계 과잉물성

(a) 클로로포름(1)/n-헵탄(2)

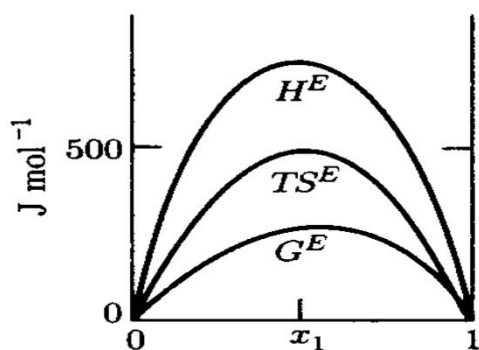
(c) 아세톤(1)/ 클로로포름(1)

(e) 에탄올(1)/ 클로로포름(2)

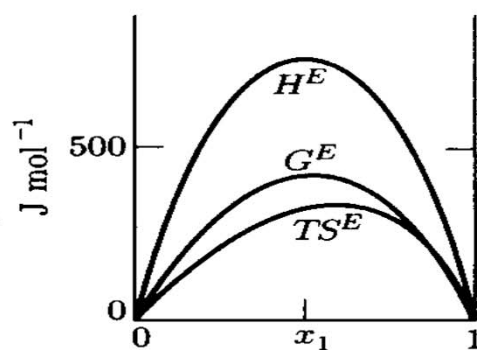
(b) 아세톤(1)/메탄올(2)

(d) 에탄올(1)/ n-헵탄(2)

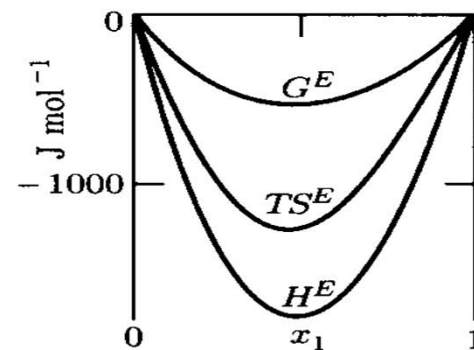
(f) 에탄올(1)/ 물(2)



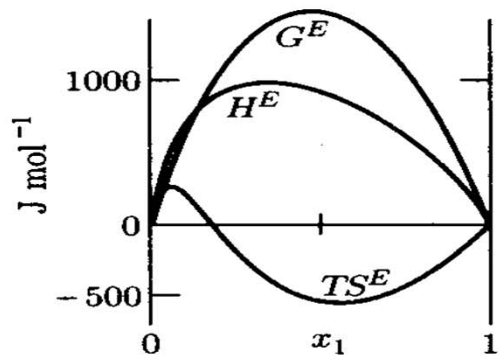
(a)



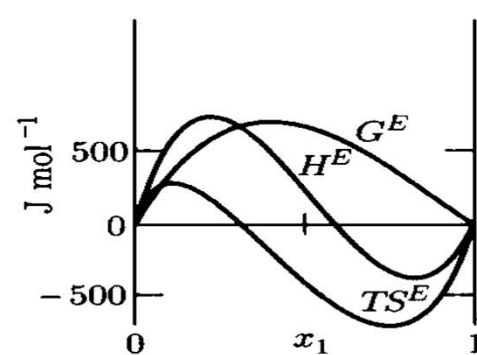
(b)



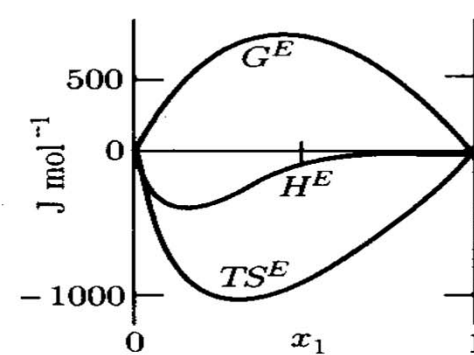
(c)



(d)



(e)

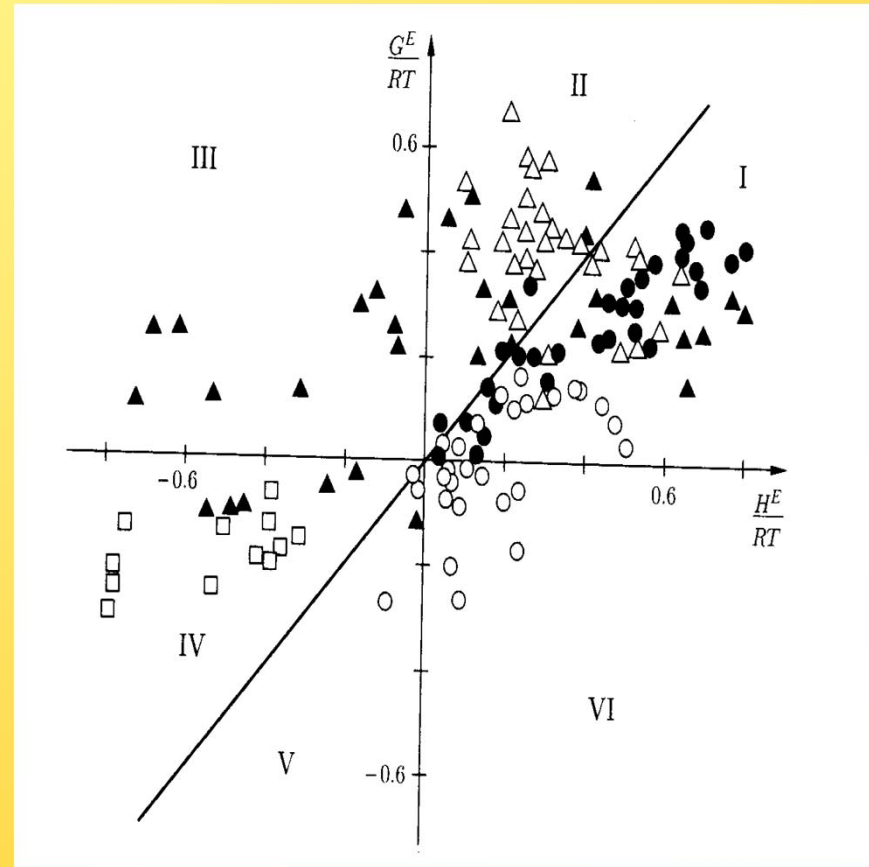


(f)

# Trends for equimolar mixtures ( 298K의 2성분계 )

[그림설명]

- : NP/NP 혼합물
- : NA/NP 혼합물
- △: AS/NP 혼합물
- ▲: AS/NA 혼합물과  
AS/AS 혼합물
- : 용매화 NA/NA  
혼합물





## II. Wohl's Expansion for the Excess Gibbs Energy

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### ■ Wohl's Expansion

$$\frac{g^E}{RT(x_1q_1 + x_2q_2)} = 2a_{12}z_1z_2 + 3a_{112}z_1^2z_2 + 3a_{122}z_1z_2^2 + 4a_{1112}z_1^3z_2 + 4a_{1222}z_1z_2^3 + 6a_{1122}z_1^2z_2^2$$
$$z_1 = \frac{x_1q_1}{x_1q_1 + x_2q_2}, z_2 = \frac{x_2q_2}{x_1q_1 + x_2q_2}$$

### ① van Laar Equation

$$\frac{g^E}{RT} = \frac{2a_{12}x_1x_2q_1q_2}{x_1q_1 + x_2q_2}$$





# ■ Wohl's Expansion

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## ② Margules Equation

$$\ln \gamma_1 = A' x_2^2 + B' x_2^3 + C' x_2^4$$

$$\ln \gamma_2 = \left(A' + \frac{3}{2}B' + 2C'\right)x^2 - \left(B' + \frac{8}{3}C'\right)x_1^3 + C' x_1^4$$

## ③ Scatchard-Hamer Equation

$$\ln \gamma_1 = A' z_2^2 + B' z_2^3$$

$$\ln \gamma_2 = \left(A' + \frac{3}{2}B'\right)\left(\frac{v_2}{v_1}\right)z_1^2 - B'\left(\frac{v_2}{v_1}\right)z_1^3$$



# III. Wilson, NRTL, and UNIQUAC Equations

## (1) Wilson Equation

- \* 개념 ... 각 성분 분자 주위의 국부적 환경이 용액  
내의 거시적인 몰용액의 특성과 다름
- \* 완전 혼합 용액에서 적용 가능

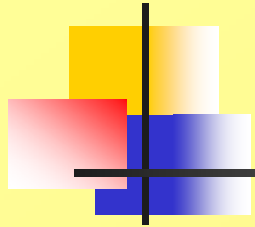
$$\frac{g^E}{RT} = -x_1 \ln(x_1 + \Lambda_{12}x_2) - x_2 \ln(x_2 + \Lambda_{21}x_1)$$

$$\ln \gamma_1 = -\ln(x_1 + \Lambda_{12}x_2) + x_2 \left( \frac{\Lambda_{12}}{x_1 + \Lambda_{12}x_2} - \frac{\Lambda_{21}}{x_2 + \Lambda_{21}x_1} \right)$$

$$\ln \gamma_2 = -\ln(x_2 + \Lambda_{21}x_1) - x_1 \left( \frac{\Lambda_{12}}{x_1 + \Lambda_{12}x_2} - \frac{\Lambda_{21}}{x_2 + \Lambda_{21}x_1} \right)$$

$$\Lambda_{12} = \frac{v_2}{v_1} \exp\left(-\frac{\lambda_{12} - \lambda_{11}}{RT}\right)$$

$$\Lambda_{21} = \frac{v_1}{v_{12}} \exp\left(-\frac{\lambda_{21} - \lambda_{22}}{RT}\right)$$



## (2) NRTL Equation

\* 완전한 혼합 성계와 불완전한 혼합의 적용

$$\frac{g^E}{RT} = x_1 x_2 \left( \frac{\tau_{21} G_{21}}{x_1 + x_2 G_{21}} + \frac{\tau_{12} G_{12}}{x_2 + x_1 G_{12}} \right)$$

$$\tau_{12} = \frac{g_{12} - g_{22}}{RT}$$

$$\tau_{21} = \frac{g_{21} - g_{11}}{RT}$$

$$G_{12} = \exp(-\alpha_{12} \tau_{12})$$

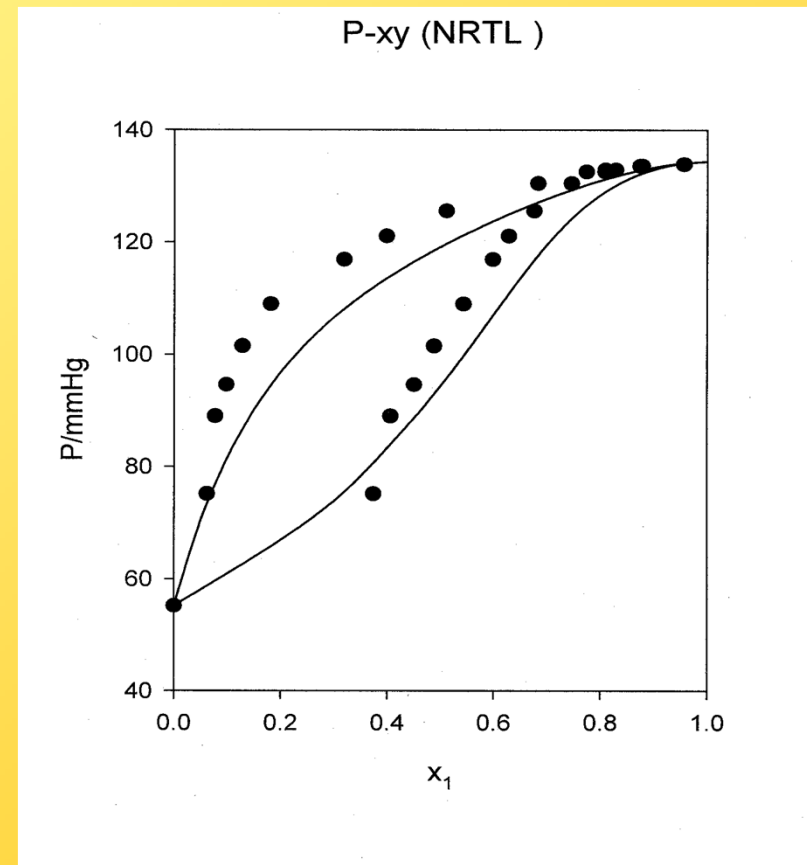
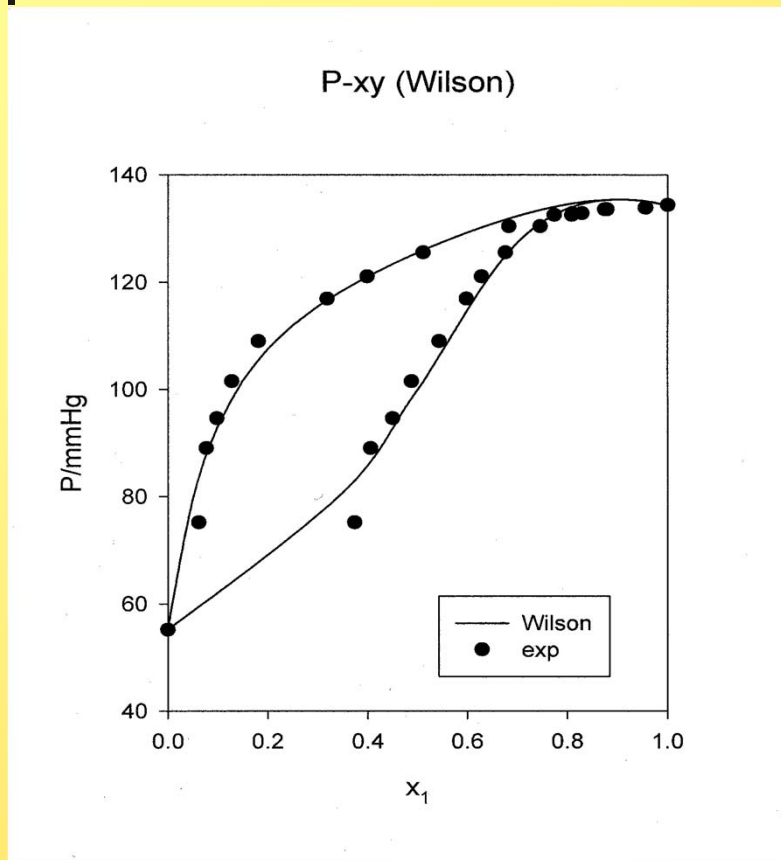
$$G_{21} = \exp(-\alpha_{12} \tau_{21})$$

$$\ln \gamma_1 = x_2^2 \left( \tau_{21} \left( \frac{G_{21}}{x_1 + x_2 G_{21}} \right)^2 + \frac{\tau_{12} G_{12}}{(x_2 + x_1 G_{12})^2} \right)$$

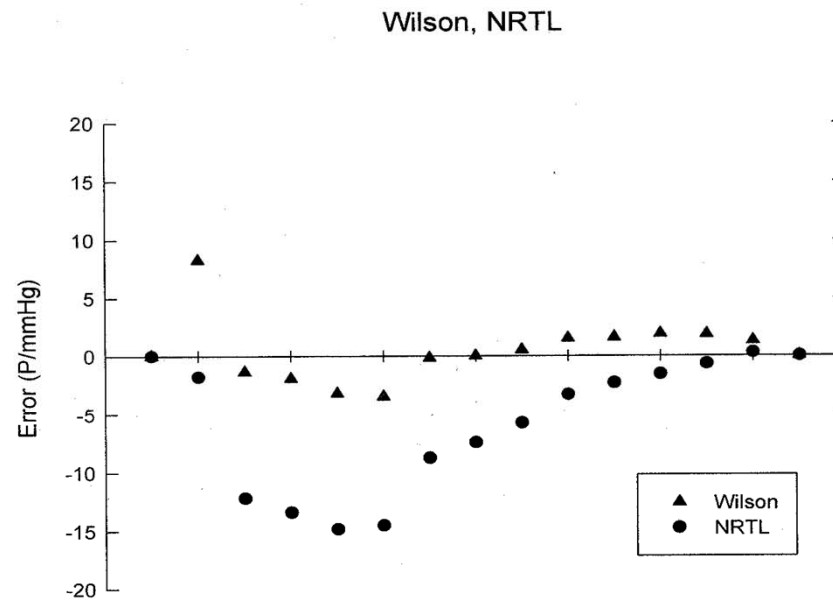
$$\ln \gamma_2 = x_1^2 \left( \tau_{12} \left( \frac{G_{12}}{x_2 + x_1 G_{12}} \right)^2 + \frac{\tau_{21} G_{21}}{(x_1 + x_2 G_{21})^2} \right)$$

# Wilson Equation과 NRTL Equation의 비교

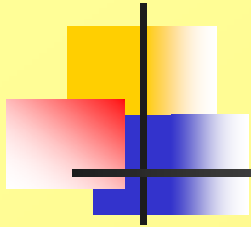
[ system : ethanol(1) / water(2) ]



# Wilson Equation과 NRTL Equation의 비교

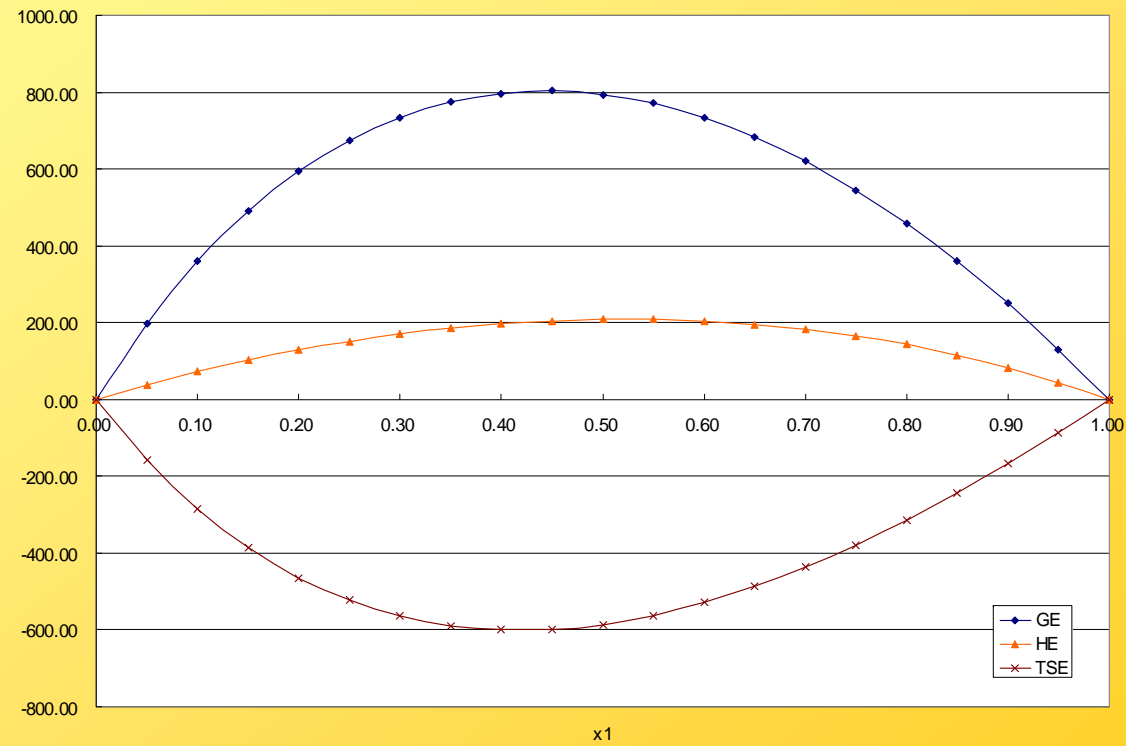


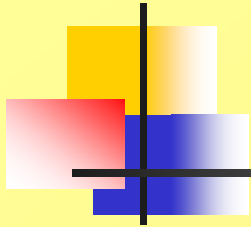
\* NRTL 식은 parameter가 3개임에도 불구하고 Wilson식이 더 오차가 적은 것을 볼 수 있다.



# Wilson Equation과 NRTL Equation의 비교

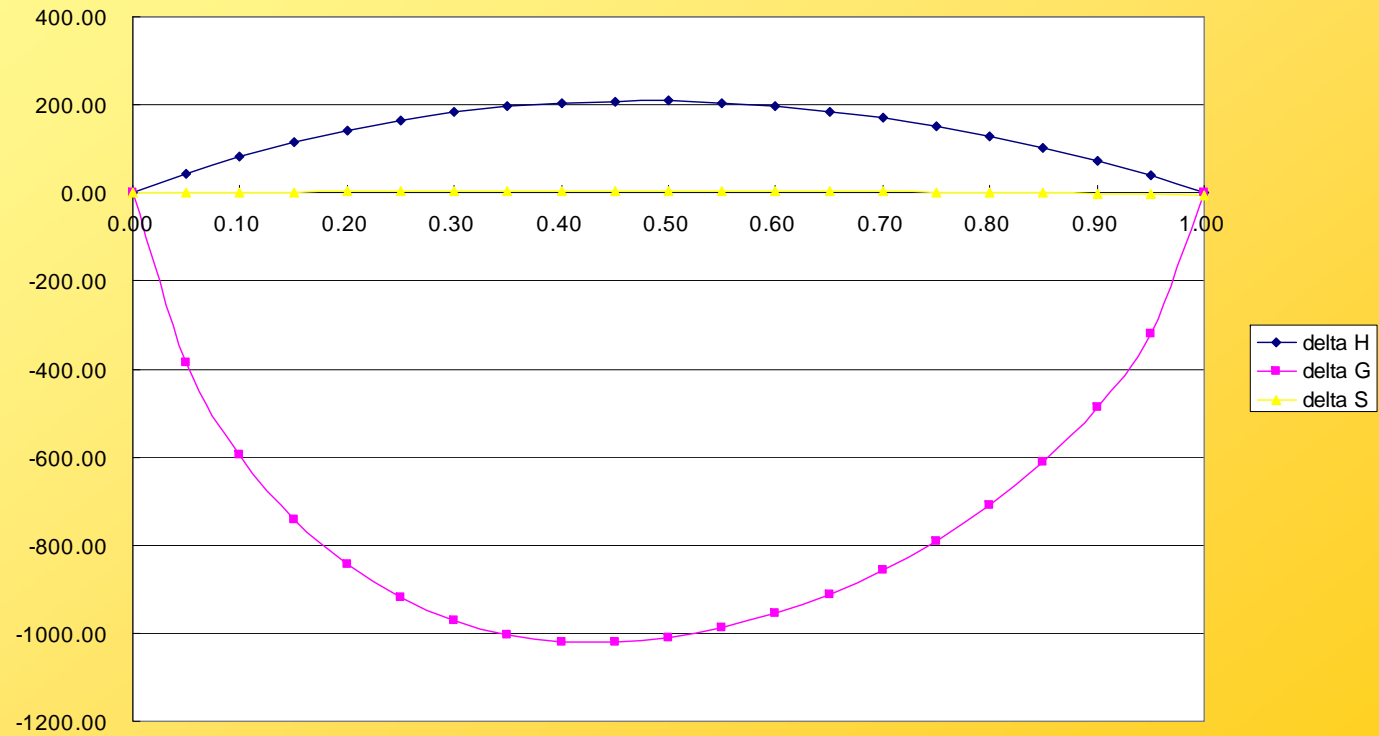
Excess property





# Wilson Equation과 NRTL Equation의 비교

energy change of mixing





### (3) UNIQUAC Equation

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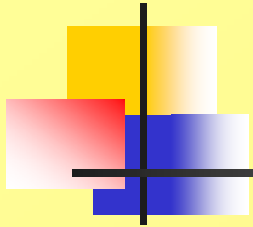
- \* 극성 , 무극성 , partial miscible mixture에서도 적용
- \* 단지 2개의 adjustable parameter만으로도 대부분의 경우에 잘 만족시킴

$$\frac{g^E}{RT} = \left( \frac{g^E}{RT} \right)_{\text{combinatorial}} + \left( \frac{g^E}{RT} \right)_{\text{residual}}$$

$$\left( \frac{g^E}{RT} \right)_{\text{combinatorial}} = x_1 \ln \frac{\Phi_1^*}{x_1} + x_2 \ln \frac{\Phi_2^*}{x_2} + \frac{z}{2} \left( x_1 q_1 \ln \frac{\theta_1}{\Phi_1^*} + x_2 q_2 \ln \frac{\theta_2}{\Phi_2^*} \right)$$

$$\left( \frac{g^E}{RT} \right)_{\text{residual}} = -x_1 q_1 \ln(\theta_1 + \theta_2 \tau_{21}) - x_2 q_2 \ln(\theta_2 + \theta_1 \tau_{12})$$





## [ The definitions of parameters ]

$$\Phi_1^* = \frac{x_1 r_1}{x_1 r_1 + x_2 r_2}$$

$$\Phi_2^* = \frac{x_2 r_2}{x_1 r_1 + x_2 r_2}$$

$$\theta_1 = \frac{x_1 q_1}{x_1 q_1 + x_2 q_2}$$

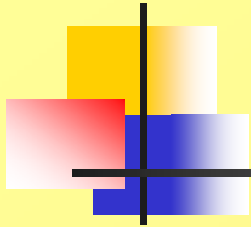
$$\theta_2 = \frac{x_2 q_2}{x_1 q_1 + x_2 q_2}$$

$$\theta_1' = \frac{x_1 q_1'}{x_1 q_1' + x_2 q_2'}$$

$$\theta_2' = \frac{x_2 q_2'}{x_1 q_1' + x_2 q_2'}$$

$$\tau_{12} = \exp\left(-\frac{\Delta u_{12}}{RT}\right) \equiv \exp\left(-\frac{a_{12}}{T}\right)$$

$$\tau_{21} = \exp\left(-\frac{\Delta u_{21}}{RT}\right) \equiv \exp\left(-\frac{a_{21}}{T}\right)$$



## UNIQUAC Equation

$$\ln \gamma_1 = \ln \frac{\Phi_1^*}{x_1} + \frac{z}{2} q_1 \ln \frac{\theta_1}{\Phi_1^*} + \Phi_2^* \left( l_1 - \frac{r_1}{r_2} l_2 \right) - q_1' \ln(\theta_1' + \theta_2' \tau_{21}) + \theta_2' q_1' \left( \frac{\tau_{21}}{\theta_1' + \theta_2' \tau_{21}} - \frac{\tau_{12}}{\theta_2' + \theta_1' \tau_{12}} \right)$$

$$\ln \gamma_2 = \ln \frac{\Phi_2^*}{x_2} + \frac{z}{2} q_2 \ln \frac{\theta_2}{\Phi_2^*} + \Phi_1^* \left( l_2 - \frac{r_2}{r_1} l_1 \right) - q_2' \ln(\theta_2' + \theta_1' \tau_{12}) + \theta_1' q_2' \left( \frac{\tau_{12}}{\theta_2' + \theta_1' \tau_{12}} - \frac{\tau_{21}}{\theta_1' + \theta_2' \tau_{21}} \right)$$

$$l_1 = \frac{z}{2} (r_1 - q_1) - (r_1 - 1)$$

$$l_2 = \frac{z}{2} (r_2 - q_2) - (r_2 - 1)$$

- [ Merits of UNIQUAC Equation ] ...
- ❶ (relative) simplicity
  - ❷ only two adjustable parameter
  - ❸ wide range of applicability



# [참고] Activity models

## Equations of State

Pen-Robinson property package option은 PR.Sour PR, PRSV입니다.  
Soave-Redlich-Kwong equation of state option은 SRK.Sour SRK, KD, ZJ입니다.

## Activity Models

Application	Margules	van Laar	Wilson	NRTL	UNIQUAC
Binary Systems	A	A	A	A	A
Multicomponent System	LA	LA	A	A	A
Azeotropic Systems	A	A	A	A	A
Liquid-Liquid Equilibria	A	A	N/A	A	A
Dilute Systems	?	?	A	A	A
Self-Associating Systems	?	?	A	A	A
Polymers	N/A	N/A	N/A	N/A	A
Extrapolating	?	?	G	G	G

- A = Application
- N/A = Not Application
- ? = Questionable
- G = Good
- LA = Limited Application